

Appendix A

**Testing Procedures and Measurement
Frequency/Protocol**

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Table A-1. Measurements for cold bench-scale tests—chemical oxidation.

Measurement/Observation	Traceability to Test Objectives	Matrix	Sample Frequency	Sample Location	Proposed Method
Weight of reaction flask	TO 2	N/A	Before test	Reaction flask	Balance
Weight of surrogate components	TO 2	Liquid/solid	Before addition to reaction flask	Weighing paper/bottle	Balance
VOCs in surrogate	TO 2	Surrogate emulsion	After surrogate is generated	Surrogate storage container	Gravimetric determination
SVOCs in surrogate	TO 2	Surrogate emulsion	After each batch of surrogate is generated	Surrogate storage container	Gravimetric determination
PCBs in surrogate	TO 2	Surrogate emulsion	After each batch of surrogate is generated	Surrogate storage container	Gravimetric determination
Metals in surrogate	TO 2	Surrogate emulsion	After each batch of surrogate is generated	Surrogate storage container	Gravimetric determination
Mercury in surrogate	TO 2	Surrogate emulsion	After each batch of surrogate is generated	Surrogate storage container	Gravimetric determination
Initial volume of surrogate	TO 2	Surrogate emulsion	Before test	Reaction flask	Graduated cylinder
Initial weight of surrogate	TO 2	Surrogate emulsion	Before test	Reaction flask	Balance
Temperature of fluid bath/ temperature of fluid entering flask jacket	TO 3	Liquid	Every 15 minutes during test	Fluid bath readout/thermometer in fluid bath	Thermometer
Temperature of water exiting flask jacket	TO 3	Liquid	Every 15 minutes during test	Exit of flask fluid jacket at return to bath	Thermometer
Flow rate of fluid circulating through jacket	TO 3	Liquid	Before each test	Fluid exiting flask into bath	Graduate cylinder/stopwatch
Temperature of cooling water at reflux condenser inlet	TO 3	Liquid	Every 15 minutes during test	Reflux condenser inlet	Thermometer

Table A-1. (continued).

Measurement/Observation	Traceability to Test Objectives	Matrix	Sample Frequency	Sample Location	Proposed Method
Temperature of cooling water at reflux condenser outlet	TO 3	Liquid	Every 15 minutes during test	Reflux condenser outlet	Thermometer
Flow through reflux condenser	TO 3	Liquid	Before each test	Fluid exiting fluid bath	Graduate cylinder/stopwatch
pH in reaction flask	TO 10	Surrogate emulsion	While adding acid to adjust pH, every 5 minutes during test duration, every minute during excursions	Two probes in reaction flask	pH meter
Temperature in reaction flask	TO 10	Surrogate emulsion	While adding acid to adjust pH, every 5 minutes during test duration, every minute during excursions	Two probes in reaction flask	Thermistor in pH meter
Chloride ion	TO 10	Surrogate emulsion	End of test	Reaction flask	ISE for chloride
Oxidizer flow rate	TO 2, TO 7, TO 8	Liquid	Every 15 minutes during test	Syringe pump	Syringe pump readout
Time interval for each oxidizer flow rate change	TO 2, TO 7, TO 8	N/A	Each time oxidizer flow rate changes	Laboratory clock	Difference in time from interval start to finish
Additions of other reagents to reaction flask (pH adjusters/catalysts, etc.)	TO 2	Liquid/solid	Before every addition, determine weight added.	Transfer container	Balance
Noncondensable gas flow rate at outlet of Dewar condenser	TO 4, TO 9	Gas	Every 10 minutes during test	Bubble meter at apparatus outlet	Bubble meters and mass flow meter
Gas at outlet of Dewar condenser	TO 4, TO 9	Gas	Every 10 minutes during test	Bubble meter at apparatus outlet	Thermocouple
Barometric pressure	TO 3	Air	Daily during testing	Laboratory barometer	Barometer
Ambient temperature	TO 3	Air	Daily during testing	Laboratory thermometer	Thermometer

Table A-1. (continued).

Measurement/Observation	Traceability to Test Objectives	Matrix	Sample Frequency	Sample Location	Proposed Method
Gas composition	TO 4, TO 9	Gas	Every 15 minutes during test or more frequently, if possible	Septum at outlet of reflux condenser	EPA Method 18 GC/TCD or GC/MS
Noncondensable gas composition	TO 4, TO 9	Gas	Every 15 minutes during test	Septum at outlet of Dewar condenser	EPA Method 18 GC/TCD or GC/MS
Time to complete test	TO 2, TO 7	N/A	Record the time of test start and finish.	Laboratory clock	Difference in time to nearest minute
Final weight of condensate	TO 4, TO 9	Liquid	After test	Condenser receiving flask	Gravimetric determination
Final weight of surrogate reaction products	TO 2, TO 7	Reacted surrogate	After test	Reaction flask contents	Gravimetric determination
Final volume of surrogate reaction products	TO 2, TO 7	Reacted surrogate	After test	Reaction flask contents	Graduated cylinder
VOCs in surrogate reaction products	TO 2, TO 7	Reacted surrogate	After test	Reaction flask	SW-846 8260B
SVOCs in surrogate reaction products	TO 2, TO 7	Reacted surrogate	After test	Reaction flask	SW-846 8270C
PCBs in surrogate reaction products	TO 2, TO 7	Reacted surrogate	After test	Reaction flask	SW-846 8082
Metals in surrogate reaction products	TO 2, TO 7	Reacted surrogate from definitive runs	After test	Reaction flask	SW-846 3050B and 6010B
Mercury in surrogate reaction products	TO 2, TO 7	Reacted surrogate	After test	Reaction flask	SW-846 7470
DRE	TO 2, TO 7, overall objective	N/A	After test	N/A	Calculation from initial and final concentrations of CFTs
Condensate composition	TO 4, TO 9	Condensate	After test	Condenser receiving flask	SW-846 8260B
Weight of reaction flask	TO 2	N/A	After decanting contents of flask	Reaction flask after test	Gravimetric determination

Table A-2. Measurements for corrosion tests.

Measurement/Observation	Traceability to Test Objectives	Matrix	Sample Frequency	Sample Location	Proposed Method
Initial weight of coupon	TO 5	Solid	Before adding to reaction flask	Material coupons	Gravimetric determination
Final weight of coupon	TO 5	Solid	After corrosion test	Material coupons	Gravimetric determination
Visual inspection/photographing coupons	TO 5	Solid	Before/after corrosion test	Material coupons	Visual

Table A-3. Measurements for bench-scale cold tests—stabilization of reaction products.

Measurement/Observation	Traceability to Test Objectives	Matrix	Sample Frequency	Sample Location	Proposed Method
Storage/cure temperature	LDR achievement	Stabilized, reacted surrogate	Daily during cure time	Water bath	Water bath/thermometer
Storage/cure time	LDR achievement	Stabilized, reacted surrogate	Elapsed time for curing	Laboratory clock	Laboratory clock
Ratio of waste to grout	LDR achievement	Stabilized, reacted surrogate	While preparing stabilized, reacted product	Grout mixing container	Gravimetric determination/calculation
TCLP Metals (Cr and Hg)	UTS for disposal	Stabilized, reacted surrogate	After 7-day cure	Cured grout	SW-846 1311
Paint filter test	ICDF waste acceptance criteria	Stabilized, reacted surrogate from definitive runs	After 30-day cure	Cured grout	SW-846 9095
Compressive strength	ICDF waste acceptance criteria	Stabilized, reacted surrogate from definitive runs	After 30-day cure	Cured grout	Handheld penetrometer

CFT = contaminant for treatment.
DO = dissolved oxygen.
DRE = destruction and removal efficiency.
EPA = U.S. Environmental Protection Agency.

GC = gas chromatograph.
ICDF = INEEL CERCLA Disposal Facility.
ISE = ion selective electrode.
LDR = land disposal restriction.

MS = mass spectrometer.
PCB = polychlorinated biphenyl.
SVOC = semivolatile organic compound.
TCD = thermal conductivity detector.

TCLP = toxicity characteristic leaching procedure.
TO = test objective.
UTS = universal treatment standard.
VOC = volatile organic compound.

Appendix B

Computational Methods and Examples

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Computational Methods and Examples

TO 2: Determine Conversion Extent of CFT Destruction

The conversion of the contaminants for treatment (CFTs) is only partially determined by the data available from the test results. DRE, destruction-removal efficiency, is easily determined, although not with a high degree of precision, by comparing the mass of each CFT in the product slurry with that charged to the reaction flask.

For example, in Run F9a, the CFTs are trichloroethylene (TCE) tetrachloroethylene (PCE), trichloroethane (TCA), bis-ethylhexylphthalate (BEHP), hexachlorobenzene (HCB), and biphenyl (BP). Hexachlorobenzene and biphenyl are substitutes for Arochlor 1260 in most of the runs; however, in the final formal runs Arochlor is added to the reaction flask, also.

As calculated in the Excel spreadsheet used to enumerate the results of each formal test (surrogateSTK.xls), the formula for DRE calculation is:

$$\text{DRE} = 100\% (1 - M_{\text{CFT } f} / M_{\text{CFT } i})$$

$M_{\text{CFT } f}$ is the mass of the compound in the products of the reaction. The mass is determined by the concentration of compound as analyzed by BWXT and by the mass of the product slurry as measured by MSE Technology personnel:

$$M_{\text{CFT } f} = [\text{CFT}] M_f / (1,000 \text{ gm/kg})$$

The concentration of the contaminant of concern, $[\text{CFT}]$, is in units of milligram of compound per kilogram of final product (mg/kg) in the Excel spreadsheet. The mass of the product slurry, M_f , is in grams. The reported quantity of the CFT is in units of total milligram in the product slurry.

$M_{\text{CFT } i}$ is the amount of the compound charged to the reaction flask. Each volatile and semivolatile compound that is charged to the reaction flask is weighed on an analytical balance using weighing paper, weighing boats or microliter syringes.

The DRE determination for each CFT is then based on the weight charged to the reaction flask, the final product weight and the analysis of the compound (ppm_w) in the product slurry. The equation expressing this result is, then:

$$\text{DRE} = 100\% \{1 - ([\text{CFT}] M_f / (1,000 \text{ gm/kg})) / M_{\text{CFT } i}\}$$

For semivolatile compounds, the above equation calculates both the DRE and percent conversion of the compound during the course of reaction. For volatile compounds, the equation calculates the DRE, but, not necessarily, the conversion by reaction. Conversion of volatile compounds has to take into account the loss of volatiles from the reaction flask by volatilization.

Test MV, the method validation test, reported DREs for TCE of 99.98%, for PCE of 99.6% and for TCA of 99.7%. The method validation test heated the standard reaction flask charge to 80°C for 8 hr. No peroxide was added to the flask during Test MV; oxygen was bubbled through the flask at about 200 acm.

Test MV showed that the volatile compounds would leave the reactor, and that DRE essentially consists of volatilization. The sparse GC/MS results available for runs F-6 (40°C, 500 mL H₂O₂) and F-13 (40°C, 400 mL H₂O₂, 12 hr) and F-21 (80°, 250 mL H₂O₂, 8 hr) indicate that the volatiles occur at low, consistent concentrations in the off-gas throughout the 40°C runs; but appear in high concentrations early in the 80°C test and diminish rapidly as the run proceeds.

Uncertainty Analysis

For a result “r,” calculated by a function such as $r = r(x, y, z)$, the general method for determining uncertainty in the result is^a:

$$[U_r]^2 = [(\partial r / \partial x) U_x]^2 + [(\partial r / \partial y) U_y]^2 + [(\partial r / \partial z) U_z]^2$$

Where U_r is the uncertainty in the result and U_x , U_y and U_z are the respective uncertainties in the independent variables.

The equation for the DRE is rewritten below to facilitate error analysis:

$$1 - \text{DRE} = ([\text{CFT}] M_f / (1,000 \text{ gm/kg})) / M_{\text{CFT } i}$$

The partial derivatives for the right hand term are:

$$(\partial[1 - \text{DRE}] / \partial[\text{CFT}]) = M_f / (1,000 \text{ gm/kg}) / M_{\text{CFT } i}$$

$$(\partial[1 - \text{DRE}] / \partial M_f) = ([\text{CFT}] / (1,000 \text{ gm/kg})) / M_{\text{CFT } i}$$

$$(\partial(1 - \text{DRE}) / \partial M_{\text{CFT } i}) = -(M_f [\text{CFT}] / (1,000 \text{ gm/kg})) / (M_{\text{CFT } i})^2$$

The uncertainty equation then becomes:

$$\begin{aligned} U_{(1 - \text{DRE})}^2 &= \{U_{[\text{CFT}]} / M_f / (1,000 \text{ gm/kg}) / M_{\text{CFT } i}\}^2 \\ &+ \{U_{M_f} / ([\text{CFT}] / (1,000 \text{ gm/kg})) / M_{\text{CFT } i}\}^2 \\ &+ \{M_{\text{CFT } i}\}^2 \end{aligned}$$

Dividing through the left hand side of the uncertainty equation by:

$$[1 - \text{DRE}]^2$$

and the right hand side by:

$$\{[\text{CFT}] M_f / (1,000 \text{ gm/kg}) / M_{\text{CFT } i}\}^2$$

simplifies the expression to:

$$\{U_{(1 - \text{DRE})} / (1 - \text{DRE})\}^2 = \{U_{[\text{CFT}]} / [\text{CFT}]\}^2 + \{U_{M_f} / M_f\}^2 + \{M_{\text{CFT } i} / M_{\text{CFT } i}\}^2$$

a. *Experimentation and Uncertainty Analysis for Engineers*; Hugh W. Coleman, W. Glen Steele, Jr.; John Wiley and Sons; 1989.

The above-simplified form of the uncertainty equation will be used for the succeeding sections of this report without derivation.

The following are the estimated uncertainties of the independent variables:

$$U_{[CFT]}/[CFT] = \pm 20\% = 0.2$$

$$U_{M_f} = \pm 0.1 \text{ g/2}$$

$$M_f = 619.4 \text{ g [test F-16 (80°, 500 mL H}_2\text{O}_2\text{, 12 hr)]}$$

$$U_{M_f}/M_f = \pm 0.05/619.4 = 80.7 \text{ E-6}$$

$$U_{M_{CFTI}} = \pm 0.0001 \text{ g/2}$$

$$M_{CFTI} = \pm 0.1656 \text{ (TCE, test F-16)}$$

$$U_{M_{CFTI}}/M_{CFTI} = \pm 0.00005 / .1656 = 302 \text{ E-6}$$

$$\{U_{(1-DRE)}/(1-DRE)\}^2 = \{0.2\}^2 + \{80.7 \text{ E-6}\}^2 + \{302 \text{ E-6}\}^2 = 40.0 \text{ E-3} = 0.04$$

$$\{U_{(1-DRE)}/(1-DRE)\} = (0.04)^{0.5} = 0.2 = 20\%$$

The final estimate of the uncertainty of the DRE calculation pretty much shows that the entire uncertainty is due to the uncertainty of the chemical analyses, or about $\pm 20\%$.

TO 3: Estimate the Rate of Heat Generation

In order for the contents of the reaction flask to stay at a steady temperature, heat generated by reaction, and heat added by the silicon oil, has to be lost through the reflux condenser and the glass surface of the flask. The energy of the flask contents is also slightly affected by the enthalpy of the peroxide stream entering the flask, and the enthalpy of the vapor stream leaving it.

The following defines the variables used in determining the heat balance:

ΔH_g : heat generated by reaction in the flask in calories per minute;

ΔH_o : enthalpy lost by the silicone oil as it is pumped through the flask;

ΔH_{cw} : enthalpy gained by the condenser water in calories per minute;

ΔH_p : enthalpy gained by the peroxide entering the flask;

ΔH_g : enthalpy of the gas leaving the reflux condenser;

Q_c : heat lost by the gas as it transits the reflux condenser;

Q_{tt} : total heat lost by the flask through its surface.

Q_{tc} : convective heat loss from the top, unjacketed half of the flask;

Qbc: convective heat loss from the bottom-jacketed-half of the flask;

Qtr: radiative heat loss from the top of the flask;

Qbr: radiative heat loss from the bottom of the flask;

Ta: ambient room temperature;

Toi: silicone oil temperature from the oil heater;

Tor: silicone oil return temperature;

Tci: condenser water inlet temperature;

Tcr: condenser water return temperature;

Tt: flask top half surface temperature;

Tb: flask bottom half surface temperature.

Mo: silicone oil flow rate;

Mc: condenser water flow rate;

Mp: peroxide flow rate;

Mog: reflux exit gas flow rate;

Yog: volume percent water vapor in the reflux exit gas;

Cw: water specific heat;

Co: silicone oil specific heat;

ΔH_{H_2O} : latent heat of water vaporization.

The following equates the energy generated by reaction, and the energy transferred into the flask by the silicone oil and by the hydrogen peroxide, to the energy lost by convection and radiation from the surface of the flask and by transport of vapor from the flask:

$$\Delta H_g + \Delta H_o + \Delta H_p = Q_{tt} + Q_c + \Delta H_{og}$$

The overall heat balance can be rewritten as:

$$\Delta H_g = -\Delta H_o - \Delta H_p + Q_{tt} + Q_c + \Delta H_{og}$$

The enthalpy change of the oil (ΔH_o) is negative since the oil cools. The oil enthalpy change is calculated by:

$$\Delta H_o = M_o C_o (T_{or} - T_{oi})$$

The enthalpy change of the condenser water (ΔH_{cw}) is a positive number, since the water heats up. The condenser water enthalpy change is subtracted from the energy in the flask since it represents heat taken away from the flask, or, $Q_c = -\Delta H_{cw}$. The heat taken away from the flask is due to cooling of the non-condensable gas formed by reaction and by condensing the water vaporized into the gas stream. For the purpose of this analysis, it is assumed that the gas will be saturated by water vapor as it exits the reflux condenser at the temperature indicated at sample port “P2” of the glassware apparatus (Figure 2-1). The amount of heat transferred to the condenser water is:

$$\Delta H_{cw} = M_c C_w (T_{cr} - T_{ci})$$

The exit gas from the reflux condenser has been cooled to the point of having near zero enthalpy; however, there is a certain fraction of water that has vaporized into it. The energy leaving the flask due to water evaporation is accounted for by:

$$\Delta H_{og} = Y_{og} M_{og} \Delta H_{H_2O} / 31.3 \text{ g/gmol}$$

An average molecular weight of 31.3 has been estimated for the exit gas, based on it being mostly oxygen with about 5% water vapor as its main constituents.

The total heat loss through the glass surface of the flask is equal to the convective loss and radiative losses from the top of the flask, which are a function of the surface temperature of the glass, and the corresponding losses through the outer surface of the heating jacket, which are a function of the surface temperature of that portion of the flask, or:

$$Q_{tt} = Q_{tc} + Q_{tr} + Q_{bc} + Q_{br}$$

Several approaches to estimating the heat loss from the flask were made. The method validation test that was run on 21 July included all components of the surrogate but no peroxide injection; thus, any heat added to the system by the silicone oil had to be lost through the reflux condenser and glass surfaces of the flask. There should be no term for heat generation by reaction.

The upper and lower glass surface areas of the flask were estimated, and convection and radiation equations written to attempt to correlate the losses. Mathcad was used to estimate the losses. The Mathcad calculations used the surface temperatures of the flask and the ambient air temperature to estimate the heat losses. The convective heat transfer coefficient was the only correlating variable.

The heat loss equations were added to the Excel spreadsheet used to reduce the run data. It was eventually determined that a value of the convective coefficient of about 2.75 Btu/hr/ft²/°F provided a near fit to the data from the final few tests.

On the 7th and 12th of August, further attempts were made to correlate the heat loss from the reaction flask. In these tests, 500 mL of water was placed in the flask and the silicone oil used to heat it. The water to the reflux condenser cooled any resulting vapor.

The data from the heat loss runs were correlated with a linear least squares program against both oil bath temperature (T_{oi}) and oil bath temperature minus ambient temperature ($T_{oi} - T_a$). Both correlated with an $r = 0.99$.

The resulting correlations were:

$$Q_{tt} = 66.48 (T_{oi} - T_a) - 411.25 \text{ cal/min, with } T \text{ in } ^\circ\text{C}$$

$$Q_{tt} = 66.52 T_{oi} - 2324.54 \text{ cal/min}$$

At 100°C oil temperature and 25°C ambient temperature, the above correlations predict a heat loss of 4,330 and 4,570 calories per minute, respectively.

The heat losses from the correlations were used to find a heat transfer coefficient for Run F16 that would match the heat losses from the glassware in the heat loss tests. The average heat transfer coefficient for F-16 was 2.74.

Uncertainty Analysis

The uncertainty analysis for the generation of energy by the reaction system follows the method explained above. For the heat transferred to the flask by the silicone oil:

$$1. \quad \Delta H_o = M_o C_o (T_{or} - T_{oi})$$

the uncertainty equation becomes:

$$[U \Delta H_o / \Delta H_o]^2 =$$

$$[U_{M_o} / M_o]^2 + [U_{C_o} / C_o]^2 + [U_{T_{or}} / (T_{or} - T_{oi})]^2 + [U_{T_{oi}} / (T_{or} - T_{oi})]^2$$

For Run F-16 (80°C, 500 mL H₂O₂, 12 hr), the estimated values of uncertainty and values of the variables are:

$$U_{M_o} / M_o = (5 \text{ mL/min}) / 621 \text{ (mL/min)}$$

$$U_{C_o} / C_o = (0.15 \text{ cal/g/}^\circ\text{C}) / (0.4 \text{ cal/g/}^\circ\text{C})$$

$$U_{T_{or}} / (T_{or} - T_{oi}) = (3^\circ\text{C}) / (19.2^\circ\text{C})$$

$$U_{T_{oi}} / (T_{or} - T_{oi}) = (0.5^\circ\text{C}) / (19.2^\circ\text{C})$$

The above values give an uncertainty of the heat transferred from the oil of:

$$[U \Delta H_o / \Delta H_o] = 0.408 = 41\%$$

The major uncertainty, as can be seen above, is in the heat capacity of the silicone oil. All the company contacts and literature inspected to date has not shed light on the heat capacity at temperatures around 80 to 100°C for the BOSS DS fluid used in the constant temperature bath. Further work along this topic requires that we replace the BOSS oil with one that has documented physical properties.

2. $\Delta H_{cw} = M_c C_w (T_{cr} - T_{ci})$

The heat capacity of water, C_w , is a known quantity, so the uncertainty equation need not address it, and becomes:

$$[U_{\Delta H_{cw}} / \Delta H_{cw}]^2 = [U_{M_c} / M_c]^2 + [U_{T_{cr}} / (T_{cr} - T_{ci})]^2 + [U_{T_{ci}} / (T_{cr} - T_{ci})]^2$$

$$[U_{M_c} / M_c] = (5 \text{ mL/min}) / (1,069 \text{ mL/min})$$

$$[U_{T_{cr}} / (T_{cr} - T_{ci})] = (0.5^\circ\text{C}) / (1.9^\circ\text{C})$$

$$[U_{T_{ci}} / (T_{cr} - T_{ci})] = (0.5^\circ\text{C}) / (1.9^\circ\text{C})$$

the estimate of the uncertainty involved in the heat transferred to the reflux condenser is:

$$[U_{\Delta H_{cw}} / \Delta H_{cw}] = 37\%$$

This uncertainty is due to the very low temperature difference of the cooling water caused by the condenser being pinched because of concurrent flow.

3. $\Delta H_p = M_p C (T_a - T_r)$

The change in enthalpy of the peroxide is of the same form as the condenser water, so, by inspection, the uncertainty is:

$$[U_{\Delta H_p} / \Delta H_p]^2 = [U_{M_p} / M_p]^2 + [U_{T_a} / (T_a - T_r)]^2 + [U_{T_r} / (T_r - T_a)]^2$$

$$[U_{M_p} / M_p] = [0.001 \text{ mL/min} / 2 \text{ mL/min}]$$

$$[U_{T_a} / (T_a - T_r)] = [0.5^\circ\text{C} / (91.5 - 25)^\circ\text{C}]$$

$$[U_{T_r} / (T_r - T_a)] = [0.2^\circ\text{C} / (91.5 - 25)^\circ\text{C}]$$

$$[U_{\Delta H_p} / \Delta H_p] = 2.38 \%$$

4. $\Delta H_{og} = Y_{og} M_{og} \Delta H_{H_2O} / 31.3 \text{ g/gmol}$

The latent heat of water is known, so the uncertainty equation becomes:

$$[U_{H_{og}} / H_{og}]^2 = [U_{Y_{og}} / Y_{og}]^2 + [U_{M_{og}} / M_{og}]^2$$

$$[U_{Y_{og}} / Y_{og}] = (0.4 \text{ psia} / 12.1 \text{ psia}) = 3.3\%$$

$$[U_{M_{og}} / M_{og}] = 2.4\% \text{ (see the next section on TO-4)}$$

$$[U_{H_{og}} / H_{og}] = 4.1\%$$

$$5. \quad Q_{tt} = Q_{tc} + Q_{tr} + Q_{bc} + Q_{br}$$

$$Q_{tc} = U_o A_1 (T_s - T_a)$$

$$[U_{Q_{tc}} / Q_{tc}]^2 = [U_{U_o} / U_o]^2 + [U_{A_1} / A_1]^2 + [U_{T_s} / (T_s - T_a)]^2 + [U_{T_a} / (T_s - T_a)]^2$$

$$[U_{U_o} / U_o] = (0.8 \text{ Btu/hr/ft}^2/\text{°F}) / (2.75 \text{ Btu/hr/ft}^2/\text{°F}) = .291 = 29\%$$

$$[U_{A_1} / A_1] = 15\%$$

$$[U_{T_s} / (T_s - T_a)] = (3^\circ\text{C} / 48.9^\circ\text{C}) = 6.1\%$$

$$[U_{T_a} / (T_s - T_a)] = (3^\circ\text{C} / 48.9^\circ\text{C}) = 6.1\%$$

$$[U_{Q_{tc}} / Q_{tc}] = 33.8\%$$

The majority of the uncertainty in the quantity of heat lost by convection from the top of the flask is due to the uncertainty in the heat transfer coefficient and the uncertainty in the irregular area of the surface of the flask.

$$Q_{tr} = 0.1713 \varepsilon A_1 [(T_s/100)^4 - (T_a/100)^4]$$

$$[U_{Q_{tr}} / Q_{tr}]^2 = [U_{\varepsilon} / \varepsilon]^2 + [U_{A_1} / A_1]^2$$

$$+ [(U_{T_s}/100) (T_s/100)^3 / [(T_s/100)^4 - (T_a/100)^4]]^2$$

$$+ [-(U_{T_a}/100) (T_s/100)^3 / [(T_s/100)^4 - (T_a/100)^4]]^2$$

$$[U_{\varepsilon} / \varepsilon] = (0.05)$$

$$[U_{A_1} / A_1] = (0.15)$$

$$[(U_{T_s}/100) (T_s/100)^3 / [(T_s/100)^4 - (T_a/100)^4]] = 220 \text{ E } -6$$

$$[(U_{T_a}/100) (T_s/100)^3 / [(T_s/100)^4 - (T_a/100)^4]] = - 65.5 \text{ E } -6$$

$$[U_{Q_{tr}} / Q_{tr}] = 15.9\%$$

The uncertainty of the transfer of heat from the flask by radiation is controlled by the uncertainty of the area estimate almost wholly.

The values for the bottom of the flask, Q_{bc} and Q_{br} are assumed to be the same as those calculated for the top of the flask. Therefore, for:

$$Q_{tt} = Q_{tc} + Q_{tr} + Q_{bc} + Q_{br}$$

$$[U_{Q_{tt}} / Q_{tt}]^2 = [U_{Q_{tc}} / Q_{tc}]^2 + [U_{Q_{tr}} / Q_{tr}]^2 + [U_{Q_{bc}} / Q_{bc}]^2 + [U_{Q_{br}} / Q_{br}]^2$$

$$[U_{Q_{tt}} / Q_{tt}] = 52.8\%$$

$$6. \quad \Delta H_g = -\Delta H_o - \Delta H_p + Q_{tt} + Q_c + \Delta H_{og}$$

$$[U_{\Delta H_g} / \Delta H_g]^2 =$$

$$[U_{\Delta H_o} / \Delta H_o]^2 + [U_{\Delta H_p} / \Delta H_p]^2 + [U_{Q_{tt}} / Q_{tt}]^2 + [U_{Q_c} / Q_c]^2 + [U_{\Delta H_{og}} / \Delta H_{og}]^2$$

$$[U_{\Delta H_o} / \Delta H_o] = 0.41$$

$$[U_{\Delta H_p} / \Delta H_p] = 0.023$$

$$[U_{Q_{tt}} / Q_{tt}] = 0.53$$

$$[U_{Q_c} / Q_c] = 0.37$$

$$[U_{\Delta H_{og}} / \Delta H_{og}]^2 = 0.041$$

$$[U_{\Delta H_g} / \Delta H_g] = 77\%$$

The analysis above forces the conclusion that we have virtually no certainty of the heat generated by reaction based on the method employed. The major components of uncertainty are the heat added by the oil (because of its unknown heat capacity), and the subsequent heat losses through the reflux condenser and the walls of the flask. The heat losses through the walls of the flask are not truly independent since these losses are calculated from the heat added by the oil and, therefore, are correlated to the heat added by the oil. Since the uncertainty of the heat lost is correlated to the heat added, the overall error above may be estimated high. However, there is no reason to further quantify the error since, as has been stated, the estimated heat generation rate is much greater than the heat that should be generated as calculated by thermodynamics. The only conclusion that can be drawn at this point is that the heat generated by reaction should be less than that measured in the current apparatus.

TO 4: Estimate the Bulk Gas Generation Rate

The bulk gas generation rate, M_{og} , defined as the reflux exit gas flow rate in the previous section, is determined using a "bubble-meter" and a stopwatch.

We use bubble meters graduated in 0 to 50 mL, or 0 to 10 mL, depending on the flow rate of gas from the reaction flask. If the volume measured is designated, V_{og} , and the time measured by the stopwatch is $\Delta \theta$, the grams per minute flowing from the reaction flask is calculated as:

$$M_{og} = V_{og} \rho_{og} / \Delta \theta$$

A density measurement, ρ_{og} , is required to convert the calculated accm to a mass flow rate. The ideal gas law is used along with the absolute pressure, room temperature and the estimated gas molecular weight. The Excel spreadsheet uses the measured or estimated gas composition to estimate the molecular weight. The final density equation is then:

$$\rho_{og} = P_a M_w / (R T_a)$$

with P_a and T_a indicating the absolute pressure and temperature, respectively, and R being the gas constant.

The mass flow equation is then, when put together:

$$M_{og} = V_{og} P_a M_{w_{og}} / (R T_a \Delta\theta)$$

The mass flow is a point value and is measured with the bubble meter every 15 min throughout each test run. To determine the total mass of gas from the reaction, each succeeding point value is averaged with the immediately previous point value and multiplied by the time interval between them. The calculated mass of gas between every 15 min time interval is then added to the previous sum to “integrate” the rate versus time curve.

Uncertainty Analysis

The reduced uncertainty equation is:

$$M_{og} = V_{og} P_a M_{w_{og}} / (R T_a \Delta\theta)$$

$$[U_{M_{og}} / M_{og}]^2 = [U_{V_{og}} / V_{og}]^2 + [U_{P_a} / P_a]^2 + [U_{M_{w_{og}}} / M_{w_{og}}]^2 + [U_{T_a} / T_a]^2 + [U_{\Delta\theta} / \Delta\theta]^2$$

The estimated uncertainties and absolute values from Run F-16 (80°C, 500 mL H₂O₂, 12 hr) are listed below:

$$U_{V_{og}} / V_{og} = 0.05 \text{ mL} / 50 \text{ mL}$$

$$U_{P_a} / P_a = 0.005 \text{ psi} / 12.08 \text{ psia}$$

$$U_{M_{w_{og}}} / M_{w_{og}} = (0.6 \text{ g/gmol}) / (31.3 \text{ g/gmol})$$

$$U_{T_a} / T_a = 3^\circ\text{C} / 293 \text{ K}$$

$$U_{\Delta\theta} / \Delta\theta = 0.02 \text{ sec} / 7.02 \text{ sec}$$

The above numbers give an estimated uncertainty for the bulk gas generation rate of:

$$U_{M_{og}} / M_{og} = \pm 2.4\%$$

TO 9: Determine the Behavior of VOCs in the Off-gas

The mass of volatiles exiting the reaction flask through the off-gas is estimated by multiplying the volume fraction of the particular compound (as measured by GC/MS) by the molar flowrate of the offgas. This product is then multiplied by the molecular weight of the compound. The total mass of each compound is then calculated by integrating the point values as described above.

$$M_{cft} = [CFT] M_{og} M_{w_{cft}} / M_{w_{og}}$$

Uncertainty Analysis

$$\{U_{M[CFT]} / [CFT]\}^2 = \{U_{[CFT]} / [CFT]\}^2 + [U_{Mog} / Mog]^2 + [U_{Mwog} / Mwog]^2$$

$$\{U_{[CFT]} / [CFT]\}^2 = [0.4]^2$$

The other two values have been determined in the previous section, giving an overall uncertainty for VOCs in the off-gas of about,

$$\{U_{M[CFT]} / [CFT]\} = 40.1\%$$

Appendix C

Test Run Summaries

1 of 4
C-3

2 of 4
C-4

S Kujawa 7/22/2003										
TEST RUN	MV-1									
	Results									
	Product slurry Sp. Gr.:	1.13						Str RPM:	372	
	Final Product Slurry, ml:	129								
	Final Product Slurry, gm:	146.1								
	Dewar Flask net wt., gm	0.007								
	Liquid/slurry Product, gm:	146.1			(Slurry Wt, 100% H2O2/O2 RXN):	291				
	Product Gas Weight, gm:	53.4								
	Product Wt, gm:	199.5								
	Total Charge Weight, gm:	291								
	Overall Mass Balance									
	Mass Balance Closure:	68.6%								
	Mass balance w/o gas:	89%								
	Species Mass Results				Species Mass Results					
	TriChloroEthylene				HexachloroBenzene					
	Slurry analysis, 1, mg/kg:	2.00 U								
	Slurry analysis, 2, mg/kg:	0.219 J								
	Avg., mg/kg	1.110			slurry ,mg:	tbd				
	Total, mg:	0.162								
	TCE, DRE, %	99.98%			HCb, DRE, %	#VALUE!				
	TetraChloroEthylene				Bi-Phenyl					
	Slurry analysis, 1, mg/kg:	2.00 U								
	Slurry analysis, 2, mg/kg:	1.96 U								
	Avg., mg/kg	1.980			slurry ,mg:	tbd				
	Total, mg:	0.289								
	PCE, DRE, %	99.6%			BP, DRE, %	#VALUE!			Run time:	8.0 Hours
	1,1,1-TriChloroEthane				Aroclor 1260				Run Temp:	79.9 deg C
	Slurry analysis, 1, mg/kg:	2.00 U							H2O2 vol:	0 ml
	Slurry analysis, 2, mg/kg:	1.96 U								
	Avg., mg/kg	1.980			slurry ,mg:					
	Total, mg:	0.289								
	TCA, DRE, %	99.7%			Aroclor, DRE, %	#VALUE!				
	BEHP									
	Slurry analysis, 1, mg/kg:									
	Slurry analysis, 2, mg/kg:									
	Avg., mg/kg	#DIV/0!								
	Total, mg:	#DIV/0!								
	BEHP, DRE, %	#DIV/0!								

Semivolatile samples destroyed in shipping

[illegible]

1 of 6
C-7

	S Kujawa																
	8/6/2003																
	TEST RUN	F-6															
Run Time	Gas Vol, cc	Time, sec	accm	Temp, C	P baro psia	MW	Density lb/ft^3	gm/min	Time delta min.	Rate avg gm/min	Mass delta gm	Mass sum gm					Rctr T Deg C
9:45	0	1	0	21	12.04	31.4	0.067	0.000		0.000	0.000	0.0					43.8
9:50	0	1	0	21	12.04	31.4	0.067	0.000	5.0	0.000	0.000	0.0					43.7
10:00	0	1	0	21	12.04	31.5	0.067	0.000	10.0	0.000	0.000	0.0					43.7
10:15	3	12.22	15	22	12.04	31.5	0.067	0.016	15.0	0.008	0.118	0.1					44
10:30	3	10.43	17	23.5	12.04	31.5	0.066	0.018	15.0	0.017	0.255	0.4					44.2
10:45	3	23.63	8	24	12.04	31.5	0.066	0.008	15.0	0.013	0.198	0.6					44.4
11:00	10	38.62	16	24.5	12.04	31.6	0.066	0.016	15.0	0.012	0.184	0.8					44.5
11:15	10	31.54	19	25	12.04	31.6	0.066	0.020	15.0	0.018	0.275	1.0					44.7
11:30	10	30.34	20	25	12.04	31.6	0.066	0.021	15.0	0.021	0.308	1.3					44.9
11:45	10	28.53	21	25	12.04	31.6	0.066	0.022	15.0	0.022	0.324	1.7					45
12:00	10	28.72	21	26	12.04	31.6	0.066	0.022	15.0	0.022	0.332	2.0					44.6
12:15	10	28.03	21	26	12.04	31.5	0.066	0.023	15.0	0.022	0.335	2.3					44.6
12:30	10	26.97	22	26	12.04	31.6	0.066	0.023	15.0	0.023	0.346	2.7					44.6
12:45	10	26.69	22	26	12.04	31.6	0.066	0.024	15.0	0.024	0.354	3.0					44.9
13:00	10	26.68	22	25	12.04	31.5	0.066	0.024	15.0	0.024	0.357	3.4					44.8
13:15	10	30.4	20	25	12.04	31.5	0.066	0.021	15.0	0.022	0.335	3.7					44.5
13:30	10	24.56	24	25	12.04	31.4	0.066	0.026	15.0	0.023	0.350	4.1					44.4
13:45	10	25.31	24	25	12.04	31.4	0.066	0.025	15.0	0.025	0.381	4.5					44.3
14:00	10	26.09	23	25	12.04	31.4	0.066	0.024	15.0	0.025	0.370	4.8					44.7
14:15	10	25.19	24	25	12.04	31.4	0.066	0.025	15.0	0.025	0.370	5.2					45.2
14:30	10	23.66	25	26	12.04	31.4	0.066	0.027	15.0	0.026	0.388	5.6					45.6
14:45	10	23.75	25	27	12.04	31.5	0.065	0.027	15.0	0.027	0.399	6.0					45.8
15:00	10	22.68	26	27	12.04	31.4	0.065	0.028	15.0	0.027	0.407	6.4					46
15:15	10	23.59	25	27	12.04	31.4	0.065	0.027	15.0	0.027	0.408	6.8					46.2
15:30	10	23.37	26	27	12.04	31.4	0.065	0.027	15.0	0.027	0.401	7.2					46.3
15:45	10	22.75	26	27	12.04	31.4	0.065	0.028	15.0	0.027	0.409	7.6					46.2
16:00	10	23.19	26	27	12.04	31.4	0.065	0.027	15.0	0.027	0.410	8.0					46.1
16:15	10	22.97	26	27	12.04	31.4	0.065	0.027	15.0	0.027	0.408	8.4					46
16:30	10	24.12	25	28	12.04	31.4	0.065	0.026	15.0	0.027	0.400	8.8					46
16:45	10	23.81	25	28	12.04	31.4	0.065	0.026	15.0	0.026	0.392	9.2					46
17:00	10	24.47	25	26	12.04	31.4	0.066	0.026	15.0	0.026	0.390	9.6					46.1
17:15	10	23.5	26	26	12.04	31.4	0.066	0.027	15.0	0.026	0.395	10.0					46.3
17:30	10	29.66	20	25	12.04	31.4	0.066	0.021	15.0	0.024	0.361	10.4					46.4
17:45	10	27.35	22	25	12.04	31.4	0.066	0.023	15.0	0.022	0.333	10.7					46.4
							Avg's:	0.021	480.0				10.2		Avg:		45.1

Run Time	% O2	% CO2	% H2O	% CO	PPMv TCE	PPMv PCE	PPMv TCA	MW									
9:45	95.6%	0.075%	4%	0.0010	2.6	2.0	1.2	31.4									
9:50	95.5%	0.075%	4%	0.0021	2.6	2.0	1.2	31.4									
10:00	95.3%	0.189%	4%	0.0031	39.05	2	258.1	31.5									
10:15	95.1%	0.303%	4%	0.0041	75.5	2.0	515.0	31.5									
10:30	95.2%	0.166%	4%	0.0040	152	2	216	31.5									
10:45	95.1%	0.332%	4%	0.0039	305	4	431	31.5									
11:00	94.9%	0.498%	4%	0.0038	457	6	647	31.6									
11:15	95.1%	0.362%	4%	0.0036	534	5.5	347.0	31.6									
11:30	95.1%	0.326%	4%	0.0035	601.5	4.85	327	31.6									
11:45	95.2%	0.290%	4%	0.0034	669	4.2	307.0	31.6									
12:00	95.2%	0.268%	4%	0.0033	635	3.1	289	31.6									
12:15	95.2%	0.247%	4%	0.0032	601	2.0	271.0	31.5									
12:30	95.2%	0.266%	4%	0.0031	768.5	10.35	324	31.6									
12:45	95.2%	0.285%	4%	0.0029	936	18.7	377.0	31.6									
13:00	95.3%	0.202%	4%	0.0028	603	28.4	220.6	31.5									
13:15	95.4%	0.120%	4%	0.0027	270	38.1	64.2	31.5									
13:30	95.5%	0.099%	4%	0.0024	195	28.25	45.2	31.4									
13:45	95.5%	0.078%	4%	0.0021	120	18.4	26.2	31.4									
14:00	95.5%	0.108%	4%	0.0018	135.5	18.45	28.15	31.4									
14:15	95.5%	0.139%	4%	0.0014	151	18.5	30.1	31.4									
14:30	95.5%	0.139%	4%	0.0011	151	18.5	30.1	31.4									
14:45	95.6%	0.139%	4%	0.0008	151	18.5	30.1	31.5									
15:00	95.6%	0.114%	4%	0.0007	112.25	15.55	21.2	31.4									
15:15	95.6%	0.090%	4%	0.0006	73.5	12.6	12.3	31.4									
15:30	95.6%	0.102%	4%	0.0006	69.5	12.4	12.05	31.4									
15:45	95.6%	0.113%	4%	0.0005	65.5	12.2	11.8	31.4									
16:00	95.6%	0.130%	4%	0.0004	50.9	10	9.25	31.4									
16:15	95.6%	0.147%	4%	0.0003	36.3	7.8	6.7	31.4									
16:30	95.6%	0.129%	4%	0.0003	32.2	7.3	5.6	31.4									
16:45	95.7%	0.111%	4%	0.0002	28.1	6.8	4.5	31.4									
17:00	95.7%	0.125%	4%	0.0002	25.3	6.6	4.1	31.4									
17:15	95.6%	0.139%	4%	0.0001	22.5	6.4	3.7	31.4									
17:30	95.7%	0.111%	4%	0.0001	19.6	5.9	2.85	31.4									
17:45	95.7%	0.083%	4%	0.0000	16.7	5.4	2.0	31.4									
							Avg:	31.5									

	S Kujawa 8/6/2003		Gas Phase Species Mass															
	TEST RUN		F-6															
	Instantaneous rates:							Integrated quantities:										
	O2, gm/min	CO2, g/m	H2O g/m	CO g/m	TCE g/m	PCE g/m	TCA g/m	O2, gm	CO2, gm	H2O gm	CO gm	TCE gm	PCE gm	TCA gm				
Run Time																		
9:45	0.0000	0.00E+00	0	0	0.00E+00	0.00E+00	0.00E+00	0	0	0	0	0	0	0	0	0		
9:50	0.0000	0.00E+00	0	0	0.00E+00	0.00E+00	0.00E+00	0.000	0.000	0.000	0.000	0.0E+00	0.0E+00	0.0E+00	0.0E+00	0.0E+00		
10:00	0.0000	0.00E+00	0	0	0.00E+00	0.00E+00	0.00E+00	0.000	0.000	0.000	0.000	0.00E+00	0.0E+00	0.0E+00	0.0E+00	0.0E+00		
10:15	0.0152	6.64E-05	3.78E-04	5.73E-05	4.94E-06	1.66E-07	3.42E-05	0.114	0.000	0.003	0.000	3.70E-05	1.24E-06	2.56E-04	2.56E-04	2.56E-04		
10:30	0.0177	4.25E-05	4.41E-04	6.49E-05	1.16E-05	1.81E-07	1.67E-05	0.361	0.001	0.009	0.001	1.61E-04	3.84E-06	6.38E-04	6.38E-04	6.38E-04		
10:45	0.0078	3.75E-05	1.94E-04	2.78E-05	1.02E-05	1.60E-07	1.47E-05	0.552	0.002	0.014	0.002	3.25E-04	6.40E-06	8.73E-04	8.73E-04	8.73E-04		
11:00	0.0159	1.14E-04	3.95E-04	5.48E-05	3.13E-05	4.87E-07	4.49E-05	0.730	0.003	0.018	0.003	6.36E-04	1.13E-05	1.32E-03	1.32E-03	1.32E-03		
11:15	0.0194	1.02E-04	4.83E-04	6.49E-05	4.46E-05	5.83E-07	2.94E-05	0.994	0.005	0.025	0.004	1.21E-03	1.93E-05	1.88E-03	1.88E-03	1.88E-03		
11:30	0.0202	9.51E-05	5.03E-04	6.53E-05	5.23E-05	5.34E-07	2.88E-05	1.291	0.006	0.032	0.005	1.93E-03	2.76E-05	2.31E-03	2.31E-03	2.31E-03		
11:45	0.0215	8.99E-05	5.34E-04	6.72E-05	6.18E-05	4.92E-07	2.88E-05	1.604	0.008	0.040	0.006	2.79E-03	3.53E-05	2.75E-03	2.75E-03	2.75E-03		
12:00	0.0213	8.26E-05	5.30E-04	6.43E-05	5.82E-05	3.60E-07	2.69E-05	1.924	0.009	0.048	0.007	3.69E-03	4.17E-05	3.16E-03	3.16E-03	3.16E-03		
12:15	0.0218	7.79E-05	5.43E-04	6.36E-05	5.64E-05	2.38E-07	2.58E-05	2.248	0.010	0.056	0.007	4.55E-03	4.62E-05	3.56E-03	3.56E-03	3.56E-03		
12:30	0.0227	8.70E-05	5.63E-04	6.35E-05	7.49E-05	1.28E-06	3.20E-05	2.582	0.011	0.064	0.008	5.53E-03	5.76E-05	3.99E-03	3.99E-03	3.99E-03		
12:45	0.0229	9.41E-05	5.69E-04	6.17E-05	9.21E-05	2.33E-06	3.77E-05	2.923	0.013	0.073	0.009	6.78E-03	8.47E-05	4.52E-03	4.52E-03	4.52E-03		
13:00	0.0230	6.72E-05	5.72E-04	5.95E-05	5.96E-05	3.56E-06	2.21E-05	3.268	0.014	0.081	0.010	7.92E-03	1.29E-04	4.97E-03	4.97E-03	4.97E-03		
13:15	0.0202	3.50E-05	5.02E-04	5.00E-05	2.34E-05	4.19E-06	5.65E-06	3.592	0.015	0.089	0.011	8.55E-03	1.87E-04	5.17E-03	5.17E-03	5.17E-03		
13:30	0.0251	3.58E-05	6.22E-04	5.48E-05	2.10E-05	3.85E-06	4.93E-06	3.931	0.015	0.098	0.012	8.88E-03	2.47E-04	5.25E-03	5.25E-03	5.25E-03		
13:45	0.0243	2.74E-05	6.03E-04	4.61E-05	1.25E-05	2.43E-06	2.78E-06	4.302	0.016	0.107	0.013	9.13E-03	2.94E-04	5.31E-03	5.31E-03	5.31E-03		
14:00	0.0236	3.68E-05	5.84E-04	3.78E-05	1.37E-05	2.36E-06	2.89E-06	4.661	0.016	0.116	0.013	9.33E-03	3.30E-04	5.35E-03	5.35E-03	5.35E-03		
14:15	0.0244	4.87E-05	6.05E-04	3.21E-05	1.58E-05	2.45E-06	3.20E-06	5.021	0.017	0.125	0.014	9.55E-03	3.66E-04	5.40E-03	5.40E-03	5.40E-03		
14:30	0.0259	5.17E-05	6.42E-04	2.65E-05	1.68E-05	2.60E-06	3.39E-06	5.399	0.017	0.134	0.014	9.79E-03	4.04E-04	5.45E-03	5.45E-03	5.45E-03		
14:45	0.0258	5.14E-05	6.39E-04	1.89E-05	1.67E-05	2.59E-06	3.38E-06	5.787	0.018	0.144	0.015	1.00E-02	4.43E-04	5.50E-03	5.50E-03	5.50E-03		
15:00	0.0270	4.43E-05	6.68E-04	1.77E-05	1.30E-05	2.28E-06	2.49E-06	6.182	0.019	0.154	0.015	1.03E-02	4.80E-04	5.54E-03	5.54E-03	5.54E-03		
15:15	0.0259	3.35E-05	6.42E-04	1.5E-05	8.16E-06	1.77E-06	1.39E-06	6.579	0.020	0.163	0.015	1.04E-02	5.10E-04	5.57E-03	5.57E-03	5.57E-03		
15:30	0.0262	3.82E-05	6.48E-04	1.32E-05	7.79E-06	1.76E-06	1.37E-06	6.970	0.020	0.173	0.015	1.05E-02	5.37E-04	5.59E-03	5.59E-03	5.59E-03		
15:45	0.0269	4.38E-05	6.66E-04	1.15E-05	7.54E-06	1.78E-06	1.38E-06	7.368	0.021	0.183	0.015	1.07E-02	5.63E-04	5.61E-03	5.61E-03	5.61E-03		
16:00	0.0264	4.95E-05	6.53E-04	9.25E-06	5.75E-06	1.43E-06	1.06E-06	7.767	0.021	0.193	0.016	1.08E-02	5.87E-04	5.63E-03	5.63E-03	5.63E-03		
16:15	0.0266	5.64E-05	6.59E-04	7.31E-06	4.14E-06	1.13E-06	7.75E-07	8.165	0.022	0.203	0.016	1.08E-02	6.06E-04	5.65E-03	5.65E-03	5.65E-03		
16:30	0.0253	4.71E-05	6.27E-04	5.79E-06	3.49E-06	1.00E-06	6.16E-07	8.554	0.023	0.212	0.016	1.09E-02	6.22E-04	5.66E-03	5.66E-03	5.66E-03		
16:45	0.0256	4.09E-05	6.34E-04	4.69E-06	3.08E-06	9.45E-07	5.01E-07	8.936	0.024	0.222	0.016	1.09E-02	6.37E-04	5.66E-03	5.66E-03	5.66E-03		
17:00	0.0251	4.51E-05	6.21E-04	3.44E-06	2.72E-06	8.98E-07	4.47E-07	9.317	0.024	0.231	0.016	1.10E-02	6.51E-04	5.67E-03	5.67E-03	5.67E-03		
17:15	0.0262	5.23E-05	6.48E-04	2.39E-06	2.52E-06	9.08E-07	4.21E-07	9.701	0.025	0.241	0.016	1.10E-02	6.64E-04	5.68E-03	5.68E-03	5.68E-03		
17:30	0.0208	3.32E-05	5.14E-04	9.5E-07	1.74E-06	6.65E-07	2.57E-07	10.053	0.026	0.249	0.016	0.0111	0.0007	0.0057	0.0057	0.0057		
								Sum of components=		10.36								
										VOC in gas/ VOC fed		1.29%	0.84%	5.96%				

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C-10

C-11

S Kujawa	8/7/2003								
TEST RUN	F-6								
13:25	Water Return Temp, Deg C	7.5		Oil Return Temp, Deg C	40.9				
	bucket ck volume, ml	1000		bucket ck volume, ml	100				
	Bucket ck time, sec	29.9		Bucket ck time, sec	14.28				
	Flow rate, ml/min	2007		Flow rate, ml/min	420				
	Enthalpy change, calorie/min:	5017		Enthalpy change, calorie/min:	-1369				
	Flask Top Surface Temp., C	30.5		Flask bottom Surface Temp., C	40.3				
	Flask Top Surface Temp., F	87		Flask bottom Surface Temp., F	105				
	Air Temp., F	76.1		Air Temp., F	76.1				
	Overall HT coef. Btu/hr/F/sq ft	3		Overall HT coef.	3				
	Top flask Area, in^2	188		bottom flask Area, in^2	265				
	emisivity	0.94		emisivity	0.94				
	Convective Loss, cal/min	178		Convective Loss, cal/min	659				
	Radiative Loss, cal/min	61		Radiative Loss, cal/min	236				
	Flask top Heat Loss, cal/min	238		Flask bottom Heat Loss, cal/min	896				
	Reactor Temperature, C	44.4		P1 Gas Temp. Deg C.	25				
	Peroxide Temperature, F	76.1		Gas Flow Rate, gm/min	0.023				
	Peroxide Flow Rate, ml/min	2		Water Vap. gm/min	0.0007				
	Peroxide heat Cap, cal/gm/degC	0.8		P1 loss, H2O vapor, cal/min	0.38				
	Peroxide Enthalpy Change, cal/min	38.2							
				Accumulation/Generation, cal/min	-4820				
14:35	Water Return Temp, Deg C	8.8		Oil Return Temp, Deg C	42.5				
	bucket ck volume, ml	1000		bucket ck volume, ml	100				
	Bucket ck time, sec	29.9		Bucket ck time, sec	14.28				
	Flow rate, ml/min	2007		Flow rate, ml/min	420				
	Enthalpy change, calorie/min:	7625		Enthalpy change, calorie/min:	-1128				
	Flask Top Surface Temp., C	32.8		Flask bottom Surface Temp., C	41.3				
	Flask Top Surface Temp., F	91		Flask bottom Surface Temp., F	106				
	Air Temp., F	78.8		Air Temp., F	78.8				
	Overall HT coef. Btu/hr/F/sq ft	3		Overall HT coef.	3				
	Top flask Area, in^2	188		bottom flask Area, in^2	265				
	emisivity	0.94		emisivity	0.94				
	Convective Loss, cal/min	201		Convective Loss, cal/min	639				
	Radiative Loss, cal/min	70		Radiative Loss, cal/min	231				
	Flask top Heat Loss, cal/min	271		Flask bottom Heat Loss, cal/min	870				
	Reactor Temperature, C	45.6		P1 Gas Temp. Deg C.	27				
	Peroxide Temperature, F	78.8		Gas Flow Rate, gm/min	0.026				
	Peroxide Flow Rate, ml/min	0		Water Vap. gm/min	0.0008				
	Peroxide heat Cap, cal/gm/degC	0.8		P1 loss, H2O vapor, cal/min	0.42				
	Peroxide Enthalpy Change, cal/min	0.0							
				Accumulation/Generation, cal/min	-7639				
15:19	Water Return Temp, Deg C	8.3		Oil Return Temp, Deg C	42.9				
	bucket ck volume, ml	1000		bucket ck volume, ml	100				
	Bucket ck time, sec	29.9		Bucket ck time, sec	14.28				
	Flow rate, ml/min	2007		Flow rate, ml/min	420				
	Enthalpy change, calorie/min:	6622		Enthalpy change, calorie/min:	-1068				
	Flask Top Surface Temp., C	33.6		Flask bottom Surface Temp., C	41.7				
	Flask Top Surface Temp., F	92		Flask bottom Surface Temp., F	107				
	Air Temp., F	80.6		Air Temp., F	80.6				
	Overall HT coef. Btu/hr/F/sq ft	3		Overall HT coef.	3				
	Top flask Area, in^2	188		bottom flask Area, in^2	265				
	emisivity	0.94		emisivity	0.94				
	Convective Loss, cal/min	195		Convective Loss, cal/min	614				
	Radiative Loss, cal/min	69		Radiative Loss, cal/min	224				
	Flask top Heat Loss, cal/min	264		Flask bottom Heat Loss, cal/min	837				
	Reactor Temperature, C	46.2		P1 Gas Temp. Deg C.	28				
	Peroxide Temperature, F	80.6		Gas Flow Rate, gm/min	0.027				
	Peroxide Flow Rate, ml/min	0		Water Vap. gm/min	0.0008				
	Peroxide heat Cap, cal/gm/degC	0.8		P1 loss, H2O vapor, cal/min	0.45				
	Peroxide Enthalpy Change, cal/min	0.0							
				Accumulation/Generation, cal/min	-6656				

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C-13

Note: At the end of data collection, gas was still being generated at the rate it had been throughout the run. Reaction was still occurring. STK, 8/12/03

recalibrate time?

	S Kujawa													
	8/21/2003													
	TEST RUN	F-13												
	Instantaneous rates:				Integrated quantities:									
	O ₂ gm/min	CO ₂ g/m	H ₂ O g/m	CO g/m	TCE g/m	PCE g/m	TCA g/m	O ₂ gm	CO ₂ gm	H ₂ O gm	CO gm	TCE gm	PCE gm	TCA gm
Run Time														
8:30	0.0000	0.0000	0.0000	0.0000	0.00E+00	0.00E+00	0.00E+00	0	0	0	0	0	0	0
8:35	0.0000	0.0000	0.0000	0.0000	0.00E+00	0.00E+00	0.00E+00	0.000	0.000	0.000	0.000	0.000	0.000	0.000
8:45	0.0000	0.0000	0.0000	0.0000	0.00E+00	0.00E+00	0.00E+00	0.000	0.000	0.000	0.000	0.000	0.000	0.000
9:00	0.0000	0.0000	0.0000	0.0000	0.00E+00	0.00E+00	0.00E+00	0.000	0.000	0.000	0.000	0.000	0.000	0.000
9:15	0.0000	0.0000	0.0000	0.0000	0.00E+00	0.00E+00	0.00E+00	0.000	0.000	0.000	0.000	0.000	0.000	0.000
9:30	0.0000	0.0000	0.0000	0.0000	0.00E+00	0.00E+00	0.00E+00	0.000	0.000	0.000	0.000	0.000	0.000	0.000
9:45	0.0200	0.0001	0.0005	0.0000	6.66E-06	1.29E-06	1.70E-06	0.150	0.001	0.004	0.000	0.000	0.000	0.000
10:00	0.0182	0.0001	0.0004	0.0000	1.01E-05	1.23E-06	2.62E-06	0.436	0.001	0.011	0.000	0.000	0.000	0.000
10:15	0.0243	0.0001	0.0006	0.0000	8.80E-06	1.51E-06	2.06E-06	0.755	0.003	0.019	0.000	0.000	0.000	0.000
10:30	0.0225	0.0001	0.0006	0.0000	3.75E-06	1.27E-06	5.69E-07	1.106	0.004	0.027	0.000	0.000	0.000	0.000
10:45	0.0233	0.0001	0.0006	0.0000	3.70E-06	1.90E-06	5.54E-07	1.451	0.006	0.036	0.000	0.000	0.000	0.000
11:00	0.0252	0.0001	0.0006	0.0000	3.79E-06	2.67E-06	5.58E-07	1.814	0.007	0.045	0.000	0.001	0.000	0.000
11:15	0.0263	0.0001	0.0007	0.0000	4.66E-06	2.29E-06	6.70E-07	2.201	0.009	0.054	0.000	0.001	0.000	0.000
11:30	0.0265	0.0001	0.0007	0.0000	5.39E-06	1.80E-06	7.62E-07	2.597	0.011	0.064	0.000	0.001	0.000	0.000
11:45	0.0261	0.0001	0.0006	0.0000	3.15E-06	1.54E-06	4.94E-07	2.992	0.012	0.074	0.000	0.001	0.000	0.000
12:00	0.0303	0.0001	0.0007	0.0000	1.14E-06	1.51E-06	2.77E-07	3.415	0.014	0.084	0.000	0.001	0.000	0.000
12:15	0.0288	0.0001	0.0007	0.0000	3.08E-06	1.72E-06	3.76E-07	3.858	0.016	0.095	0.000	0.001	0.000	0.000
12:30	0.0274	0.0001	0.0007	0.0000	4.82E-06	1.90E-06	4.65E-07	4.280	0.017	0.106	0.000	0.001	0.000	0.000
12:45	0.0290	0.0001	0.0007	0.0000	4.11E-06	1.67E-06	4.36E-07	4.703	0.019	0.116	0.000	0.001	0.000	0.000
13:00	0.0283	0.0001	0.0007	0.0000	3.04E-06	1.29E-06	3.69E-07	5.133	0.021	0.127	0.000	0.001	0.000	0.000
13:15	0.0275	0.0001	0.0007	0.0000	2.95E-06	1.38E-06	3.41E-07	5.551	0.023	0.137	0.000	0.001	0.000	0.000
13:30	0.0289	0.0001	0.0007	0.0000	3.10E-06	1.58E-06	3.39E-07	5.974	0.024	0.148	0.000	0.001	0.000	0.000
13:45	0.0283	0.0001	0.0007	0.0000	2.23E-06	1.42E-06	2.95E-07	6.403	0.026	0.158	0.000	0.001	0.000	0.000
14:00	0.0272	0.0001	0.0007	0.0000	1.36E-06	1.24E-06	2.49E-07	6.819	0.028	0.168	0.000	0.001	0.000	0.000
14:15	0.0259	0.0001	0.0006	0.0000	1.63E-06	1.25E-06	2.36E-07	7.218	0.029	0.178	0.000	0.001	0.000	0.000
14:30	0.0258	0.0001	0.0006	0.0000	1.96E-06	1.32E-06	2.36E-07	7.605	0.031	0.188	0.000	0.001	0.000	0.000
14:45	0.0250	0.0001	0.0006	0.0000	1.45E-06	1.17E-06	2.28E-07	7.986	0.032	0.197	0.000	0.001	0.000	0.000
15:00	0.0231	0.0001	0.0006	0.0000	9.29E-07	9.89E-07	2.11E-07	8.346	0.034	0.206	0.000	0.001	0.001	0.000
15:15	0.0229	0.0001	0.0006	0.0000	8.63E-07	1.04E-06	2.09E-07	8.691	0.035	0.215	0.000	0.001	0.001	0.000
15:30	0.0212	0.0001	0.0005	0.0000	7.46E-07	1.01E-06	1.94E-07	9.021	0.036	0.223	0.000	0.001	0.001	0.000
15:45	0.0218	0.0001	0.0005	0.0000	8.33E-07	9.67E-07	2.00E-07	9.344	0.038	0.231	0.000	0.001	0.001	0.000
16:00	0.0215	0.0001	0.0005	0.0000	8.83E-07	8.74E-07	1.96E-07	9.669	0.039	0.239	0.000	0.001	0.001	0.000
16:15	0.0199	0.0001	0.0005	0.0000	6.01E-07	7.29E-07	1.82E-07	9.979	0.040	0.247	0.000	0.001	0.001	0.000
16:30	0.0204	0.0001	0.0005	0.0000	3.93E-07	6.64E-07	1.86E-07	10.281	0.041	0.254	0.000	0.001	0.001	0.000
16:45	0.0202	0.0001	0.0005	0.0000	3.90E-07	6.59E-07	1.85E-07	10.586	0.043	0.262	0.000	0.001	0.001	0.000
17:00	0.0197	0.0001	0.0005	0.0000	3.80E-07	6.42E-07	1.80E-07	10.885	0.044	0.269	0.000	0.001	0.001	0.000
17:15	0.0184	0.0001	0.0005	0.0000	3.56E-07	6.01E-07	1.69E-07	11.171	0.045	0.276	0.000	0.001	0.001	0.000
17:30	0.0195	0.0001	0.0005	0.0000	3.76E-07	6.36E-07	1.78E-07	11.456	0.046	0.283	0.000	0.001	0.001	0.000
17:45	0.0201	0.0001	0.0005	0.0000	3.88E-07	6.56E-07	1.84E-07	11.753	0.047	0.291	0.000	0.001	0.001	0.000
18:00	0.0198	0.0001	0.0005	0.0000	3.81E-07	6.44E-07	1.81E-07	12.052	0.048	0.298	0.000	0.001	0.001	0.000
18:15	0.0203	0.0001	0.0005	0.0000	4.44E-07	6.96E-07	1.86E-07	12.353	0.050	0.306	0.000	0.001	0.001	0.000
18:30	0.0198	0.0001	0.0005	0.0000	4.84E-07	7.10E-07	1.81E-07	12.654	0.051	0.313	0.000	0.001	0.001	0.000
18:45	0.0220	0.0001	0.0005	0.0000	4.81E-07	7.52E-07	2.01E-07	12.968	0.052	0.321	0.000	0.001	0.001	0.000
19:00	0.0214	0.0001	0.0005	0.0000	4.13E-07	6.98E-07	1.96E-07	13.293	0.053	0.329	0.000	0.001	0.001	0.000
19:15	0.0211	0.0001	0.0005	0.0000	4.07E-07	6.87E-07	1.93E-07	13.612	0.054	0.337	0.000	0.001	0.001	0.000
19:30	0.0217	0.0001	0.0005	0.0000	4.19E-07	7.07E-07	1.98E-07	13.933	0.056	0.345	0.000	0.001	0.001	0.000
19:45	0.0215	0.0001	0.0005	0.0000	4.15E-07	7.01E-07	1.97E-07	14.257	0.057	0.353	0.000	0.001	0.001	0.000
20:00	0.0202	0.0001	0.0005	0.0000	3.89E-07	6.58E-07	1.84E-07	14.570	0.058	0.361	0.000	0.001	0.001	0.000
20:15	0.0213	0.0001	0.0005	0.0000	4.11E-07	6.94E-07	1.95E-07	14.881	0.060	0.368	0.000	0.001	0.001	0.000
20:30	0.0211	0.0001	0.0005	0.0000	4.07E-07	6.88E-07	1.93E-07	15.199	0.061	0.376	0.00017	0.0014	0.0007	0.0003
								O ₂ gm	CO ₂ gm	H ₂ O gm	CO gm	TCE gm	PCE gm	TCA gm
								Sum of components=			15.64			
								VOC in gas/ VOC fed				0.16%	0.99%	0.29%

Residual peroxide test shows approximately 35% in the aqueous layer

10:32	Water Return Temp, Deg C	7.8	Oil Return Temp, Deg C	42.9			
	bucket ck volume, ml	100	bucket ck volume, ml	100			
	Bucket ck time, sec	3.16	Bucket ck time, sec	15.25			
	Flow rate, ml/min	1899	Flow rate, ml/min	393			
	Enthalpy change, calorie/min:	5316	Enthalpy change, calorie/min:	-1000			
	Flask Top Surface Temp., C	34.7	Flask bottom Surface Temp., C	40			
	Flask Top Surface Temp., F	94	Flask bottom Surface Temp., F	104			
	Air Temp., F	79	Air Temp., F	79			
	Overall HT coef. Btu/hr/F/sq ft	3	Overall HT coef.	3			
	Top flask Area, in^2	188	bottom flask Area, in^2	265			
emisivty	0.94	emisivty	0.94				
Convective Loss, cal/min	254	Convective Loss, cal/min	580				
Radiative Loss, cal/min	89	Radiative Loss, cal/min	209				
Flask top Heat Loss, cal/min	344	Flask bottom Heat Loss, cal/min	789	1132			
Reactor Temperature, C	44.3	P1 Gas Temp. Deg C.	27				
Peroxide Temperature, F	79	Gas Flow Rate, gm/min	0.024	Correlated losses, cal/min		1118	
Peroxide Flow Rate, ml/min	2	Water Vap. gm/min	0.0007	Reflux Gas Delta H, cal/min		1	
Peroxide heat Cap, cal/gm/degC	0.8	P1 loss, H2O vapor, cal/min	0.39	Revised Acc/generation, cal/min		-154	
Peroxide Enthalpy Change, cal/min	34.9						
		Accumulation/Generation, cal/min	-5484				
11:35	Water Return Temp, Deg C	6.4	Oil Return Temp, Deg C	43.3			
	bucket ck volume, ml	1000	bucket ck volume, ml	100			
	Bucket ck time, sec	29.16	Bucket ck time, sec	14.91			
	Flow rate, ml/min	2058	Flow rate, ml/min	402			
	Enthalpy change, calorie/min:	2881	Enthalpy change, calorie/min:	-965			
	Flask Top Surface Temp., C	36.3	Flask bottom Surface Temp., C	40.4			
	Flask Top Surface Temp., F	97	Flask bottom Surface Temp., F	105			
	Air Temp., F	83	Air Temp., F	83			
	Overall HT coef. Btu/hr/F/sq ft	3	Overall HT coef.	3			
	Top flask Area, in^2	188	bottom flask Area, in^2	265			
emisivty	0.94	emisivty	0.94				
Convective Loss, cal/min	236	Convective Loss, cal/min	504				
Radiative Loss, cal/min	84	Radiative Loss, cal/min	184				
Flask top Heat Loss, cal/min	320	Flask bottom Heat Loss, cal/min	687	1008			
Reactor Temperature, C	45.7	P1 Gas Temp. Deg C.	29.5				
Peroxide Temperature, F	83	Gas Flow Rate, gm/min	0.027	Correlated losses, cal/min		952	
Peroxide Flow Rate, ml/min	2	Water Vap. gm/min	0.0008	Reflux Gas Delta H, cal/min		1	
Peroxide heat Cap, cal/gm/degC	0.8	P1 loss, H2O vapor, cal/min	0.44	Revised Acc/generation, cal/min		-21	
Peroxide Enthalpy Change, cal/min	33.3						
		Accumulation/Generation, cal/min	-2952				

C-19

S Kujawa									
8/11/2003									
TEST RUN	F-13			Heat Balance					
	Condenser Bath			Oil Bath					
	Set Point Temperature, Deg C	5		Set Point Temperature, Deg C	50				
Time				Boss DS oil density, gm/ml	0.895				
				Boss DS oil heat cap. cal/gm/deg C	0.4				
15:20	Water Return Temp, Deg C	7		Oil Return Temp, Deg C	40.8				
	bucket ck volume, ml	1000		bucket ck volume, ml	100				
	Bucket ck time, sec	29.37		Bucket ck time, sec	15.03				
	Flow rate, ml/min	2043		Flow rate, ml/min	399				
	Enthalpy change, calorie/min:	4086		Enthalpy change, calorie/min:	-1343				
	Flask Top Surface Temp., C			Flask bottom Surface Temp., C					
	Flask Top Surface Temp., F	32		Flask bottom Surface Temp., F	32				
	Air Temp., F			Air Temp., F	0				
	Overall HT coef. Btu/hr/F/sq ft	3		Overall HT coef.	3				
	Top flask Area, in^2	188		bottom flask Area, in^2	265				
	emisivity	0.94		emisivity	0.94				
	Convective Loss, cal/min	526		Convective Loss, cal/min	742				
	Radiative Loss, cal/min	122		Radiative Loss, cal/min	172				
	Flask top Heat Loss, cal/min	648		Flask bottom Heat Loss, cal/min	914	1562			
	Reactor Temperature, C			P1 Gas Temp, Deg C.	23				
	Peroxide Temperature, F	0		Gas Flow Rate, gm/min	0.000		Correlated losses, cal/min	1384	
	Peroxide Flow Rate, ml/min			Water Vap. gm/min	0.0000		Reflux Gas Delta H, cal/min	0	
	Peroxide heat Cap, cal/gm/degC	0.8		P1 loss, H2O vapor, cal/min	0.00		Revised Acc/generation, cal/min	-40	
	Peroxide Enthalpy Change, cal/min	0.0							
				Accumulation/Generation, cal/min	-4305				
16:40	Water Return Temp, Deg C	6.5		Oil Return Temp, Deg C	42				
	bucket ck volume, ml	1000		bucket ck volume, ml	100				
	Bucket ck time, sec	28.82		Bucket ck time, sec	16.38				
	Flow rate, ml/min	2082		Flow rate, ml/min	366				
	Enthalpy change, calorie/min:	3123		Enthalpy change, calorie/min:	-1049				
	Flask Top Surface Temp., C			Flask bottom Surface Temp., C					
	Flask Top Surface Temp., F	32		Flask bottom Surface Temp., F	32				
	Air Temp., F			Air Temp., F	0				
	Overall HT coef. Btu/hr/F/sq ft	3		Overall HT coef.	3				
	Top flask Area, in^2	188		bottom flask Area, in^2	265				
	emisivity	0.94		emisivity	0.94				
	Convective Loss, cal/min	526		Convective Loss, cal/min	742				
	Radiative Loss, cal/min	122		Radiative Loss, cal/min	172				
	Flask top Heat Loss, cal/min	648		Flask bottom Heat Loss, cal/min	914	1562			
	Reactor Temperature, C			P1 Gas Temp, Deg C.	24				
	Peroxide Temperature, F	0		Gas Flow Rate, gm/min	0.019		Correlated losses, cal/min	1317	
	Peroxide Flow Rate, ml/min	0		Water Vap. gm/min	0.0006		Reflux Gas Delta H, cal/min	1	
	Peroxide heat Cap, cal/gm/degC	0.8		P1 loss, H2O vapor, cal/min	0.31		Revised Acc/generation, cal/min	-269	
	Peroxide Enthalpy Change, cal/min	0.0							
				Accumulation/Generation, cal/min	-3636				
17:35	Water Return Temp, Deg C	6.3		Oil Return Temp, Deg C	41.8				
	bucket ck volume, ml	1000		bucket ck volume, ml	100				
	Bucket ck time, sec	28.34		Bucket ck time, sec	14.47				
	Flow rate, ml/min	2117		Flow rate, ml/min	415				
	Enthalpy change, calorie/min:	2752		Enthalpy change, calorie/min:	-1217				
	Flask Top Surface Temp., C	31.7		Flask bottom Surface Temp., C	39.6				
	Flask Top Surface Temp., F	89		Flask bottom Surface Temp., F	103				
	Air Temp., F	77		Air Temp., F	77				
	Overall HT coef. Btu/hr/F/sq ft	3		Overall HT coef.	3				
	Top flask Area, in^2	188		bottom flask Area, in^2	265				
	emisivity	0.94		emisivity	0.94				
	Convective Loss, cal/min	198		Convective Loss, cal/min	609				
	Radiative Loss, cal/min	68		Radiative Loss, cal/min	218				
	Flask top Heat Loss, cal/min	267		Flask bottom Heat Loss, cal/min	827	1094			
	Reactor Temperature, C	44.8		P1 Gas Temp, Deg C.	25				
	Peroxide Temperature, F	77		Gas Flow Rate, gm/min	0.019		Correlated losses, cal/min	1251	
	Peroxide Flow Rate, ml/min	0		Water Vap. gm/min	0.0006		Reflux Gas Delta H, cal/min	1	
	Peroxide heat Cap, cal/gm/degC	0.8		P1 loss, H2O vapor, cal/min	0.32		Revised Acc/generation, cal/min	-34	
	Peroxide Enthalpy Change, cal/min	0.0							
				Accumulation/Generation, cal/min	-2629				

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S Kujawa	8/15/2003								
					Test Results	Str RPM:		Start	
TEST RUN									
	F-20								
	Results								
	Product slurry Sp. Gr.:	1.09							
	Final Product Slurry, ml:	271							
	Final Product Slurry, gm:	295.1							
	Dewar Flask net wt., gm	0.3507							
	Liquid/slurry Product, gm:	295.5		(Slurry Wt, 100% H2O2/O2 RXN)	303				
	Product Gas Weight, gm:	41.4							
	Product Wt, gm:	336.8							
	Total Charge Weight, gm:	345							
	Overall Mass Balance								
	Mass Balance Closure:	97.5%							
	Mass balance w/o gas:	86%							
	Species Mass Results			Species Mass Results					
	TriChloroEthylene			Anal. code HexachloroBenzene		Anal. code			
	Slurry analysis, 1, mg/kg:	17.100		Slurry analysis, 1, mg/kg:	5.470				
	Slurry analysis, 2, mg/kg:	20.200		Slurry analysis, 2, mg/kg:	5.780				
	Avg., mg/kg	18.650		Avg., mg/kg	5.625				
	Total, mg:	5.504		Total, mg:	1.660				
	TCE, DRE, %	99.36%		HCb, DRE, %	72.33%				
	TetraChloroEthylene			Bi-Phenyl					
	Slurry analysis, 1, mg/kg:	2.630		Slurry analysis, 1, mg/kg:	4.730 U				
	Slurry analysis, 2, mg/kg:	3.290		Slurry analysis, 2, mg/kg:	0.523 J				
	Avg., mg/kg	2.960		Avg., mg/kg	2.627				
	Total, mg:	0.873		Total, mg:	0.775				
	PCE, DRE, %	98.76%		BP, DRE, %	73.27%		Run time:	8 Hours	
	1,1,1-TriChloroEthane			Aroclor 1260			Run Temp:	84.9 deg C	
	Slurry analysis, 1, mg/kg:	0.268 J		Slurry analysis, 1, mg/kg:	tbid		H2O2 vol:	150 ml	
	Slurry analysis, 2, mg/kg:	0.305 J		Slurry analysis, 2, mg/kg:					
	Avg., mg/kg	0.287		Avg., mg/kg	#DIV/0!				
	Total, mg:	0.085		Total, mg:	#DIV/0!				
	TCA, DRE, %	99.91%		Aroclor, DRE, %	#DIV/0!				
	BEHP								
	Slurry analysis, 1, mg/kg:	190 D							
	Slurry analysis, 2, mg/kg:	195							
	Avg., mg/kg	193							
	Total, mg:	57							
	BEHP, DRE, %	65.90%							

S Kujawa	8/15/2003	Heat Balance					
TEST RUN	F-20						
	Condenser Bath			Oil Bath			
	Set Point Temperature, Deg C	5		Set Point Temperature, Deg C	100		
	The heat balance and heat generation calculations are very uncertain due to lack of physical properties for the heating oil. Efforts are being made to determine operating heat capacities and						
				Boss DS oil density, gm/ml	0.873		
				Boss DS oil heat cap. cal/gm/deg	0.4		
8:38	Water Return Temp, Deg C	6.9		Oil Return Temp, Deg C	78.6		
	bucket ck volume, ml	1000		bucket ck volume, ml	100		
	Bucket ck time, sec	57.84		Bucket ck time, sec	9.72		
	Flow rate, ml/min	1037		Flow rate, ml/min	617		
	Enthalpy change, calorie/min:	1971		Enthalpy change, calorie/min:	-4613		
	Flask Top Surface Temp., C	71.6		Flask bottom Surface Temp., C	79.4		
	Flask Top Surface Temp., F	161		Flask bottom Surface Temp., F	175		
	Air Temp., F	70.7		Air Temp., F	70.7		
	Overall HT coef. Btu/hr/F/sq ft	2.75		Overall HT coef.	2.75		
	Top flask Area, in^2	188		bottom flask Area, in^2	265		
	emisivity	0.94		emisivity	0.94		
	Convective Loss, cal/min	1360		Convective Loss, cal/min	2215		
	Radiative Loss, cal/min	612		Radiative Loss, cal/min	1035		
	Flask top Heat Loss, cal/min	1972		Flask bottom Heat Loss, cal/min	3251	5222	
	Reactor Temperature, C	89.6		P1 Gas Temp. Deg C	23		
	Peroxide Temperature, F	70.7		Gas Flow Rate, gm/min	0.438		
	Peroxide Flow Rate, ml/min	2		Water Vap. gm/min	0.0129		
	Peroxide heat Cap, cal/gm/degC	0.8		P1 loss, H2O vapor, cal/min	7.18		
	Peroxide Enthalpy Change, cal/m	130.8					
				Accumulation/Generation, cal/min	-2718		
	Correlated losses, cal/min	4708					
	Reflux Gas Delta H, cal/min	752					
	Revised Acc/generation, cal/min	-978					
9:33	Water Return Temp, Deg C	6.8		Oil Return Temp, Deg C	78.5		
	bucket ck volume, ml	1000		bucket ck volume, ml	1000		
	Bucket ck time, sec	58.07		Bucket ck time, sec	97.63		
	Flow rate, ml/min	1033		Flow rate, ml/min	615		
	Enthalpy change, calorie/min:	1860		Enthalpy change, calorie/min:	-4614		
	Flask Top Surface Temp., C	75.2		Flask bottom Surface Temp., C	78.4		
	Flask Top Surface Temp., F	167		Flask bottom Surface Temp., F	173		
	Air Temp., F	73		Air Temp., F	73		
	Overall HT coef. Btu/hr/F/sq ft	2.75		Overall HT coef.	2.75		
	Top flask Area, in^2	188		bottom flask Area, in^2	265		
	emisivity	0.94		emisivity	0.94		
	Convective Loss, cal/min	1423		Convective Loss, cal/min	2128		
	Radiative Loss, cal/min	655		Radiative Loss, cal/min	995		
	Flask top Heat Loss, cal/min	2078		Flask bottom Heat Loss, cal/min	3123	5201	
	Reactor Temperature, C	90.8		P1 Gas Temp. Deg C	24		
	Peroxide Temperature, F	73		Gas Flow Rate, gm/min	0.363		
	Peroxide Flow Rate, ml/min	2		Water Vap. gm/min	0.0107		
	Peroxide heat Cap, cal/gm/degC	0.8		P1 loss, H2O vapor, cal/min	5.94		
	Peroxide Enthalpy Change, cal/m	130.6					
				Accumulation/Generation, cal/min	-2684		
	Correlated losses, cal/min	4641					
	Reflux Gas Delta H, cal/min	623					
	Revised Acc/generation, cal/min	-780					
10:32	Water Return Temp, Deg C	6.9		Oil Return Temp, Deg C	78		
	bucket ck volume, ml	1000		bucket ck volume, ml	1000		
	Bucket ck time, sec	58.06		Bucket ck time, sec	93.93		
	Flow rate, ml/min	1033		Flow rate, ml/min	639		
	Enthalpy change, calorie/min:	1963		Enthalpy change, calorie/min:	-4907		
	Flask Top Surface Temp., C	67.5		Flask bottom Surface Temp., C	78.4		
	Flask Top Surface Temp., F	154		Flask bottom Surface Temp., F	173		
	Air Temp., F	75.2		Air Temp., F	75.2		
	Overall HT coef. Btu/hr/F/sq ft	2.75		Overall HT coef.	2.75		
	Top flask Area, in^2	188		bottom flask Area, in^2	265		
	emisivity	0.94		emisivity	0.94		
	Convective Loss, cal/min	1181		Convective Loss, cal/min	2081		
	Radiative Loss, cal/min	526		Radiative Loss, cal/min	979		
	Flask top Heat Loss, cal/min	1707		Flask bottom Heat Loss, cal/min	3060	4767	
	Reactor Temperature, C	85.3		P1 Gas Temp. Deg C	24.5		
	Peroxide Temperature, F	75.2		Gas Flow Rate, gm/min	0.095		4608
	Peroxide Flow Rate, ml/min	2		Water Vap. gm/min	0.0028		163
	Peroxide heat Cap, cal/gm/degC	0.8		P1 loss, H2O vapor, cal/min	1.56		Revised Acc/generation, cal/min
	Peroxide Enthalpy Change, cal/m	117.7					18
				Accumulation/Generation, cal/min	-1942		

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	S Kujawa													
	8/20/2003													
	TEST RUN	F-21												
Run Time	Gas Vol, cc	Time, sec	accm	Temp, C	P baro	MW	Density	gm/min	Time delta	Rate avg	Mass delta	Mass sum		Rctr T
					psia		lb/ft^3	0	min.	gm/min	gm	gm		Deg C
9:00		1	0	22	12.08	31.5	0.067	0.000	0.0	0.000	0.00	0.0		86.6
9:05	50	12.94	232	22	12.08	31.5	0.067	0.248	5.0	0.124	0.62	0.6		85.7
9:15	50	8.25	364	21	12.08	31.5	0.067	0.391	10.0	0.320	3.20	3.8		90.1
9:30	50	7.75	387	20	12.08	31.5	0.067	0.417	15.0	0.404	6.06	9.9		91.2
9:45	50	7.78	386	21.5	12.08	31.5	0.067	0.413	15.0	0.415	6.23	16.1		90.8
10:00	50	7.53	398	22	12.08	31.5	0.067	0.426	15.0	0.420	6.30	22.4		91.4
10:15	50	7.97	376	22	12.08	31.5	0.067	0.403	15.0	0.414	6.22	28.6		90.7
10:30	50	7.75	387	23	12.08	31.5	0.067	0.413	15.0	0.408	6.12	34.7		90.4
10:45	50	7.94	378	22.5	12.08	31.5	0.067	0.403	15.0	0.408	6.12	40.9		90.7
11:00	50	10.88	276	23	12.08	31.5	0.066	0.294	15.0	0.349	5.23	46.1		88.3
11:15	50	10	300	21	12.08	31.5	0.067	0.322	15.0	0.308	4.62	50.7		90.1
11:30	50	11.1	270	24	12.08	31.5	0.066	0.287	15.0	0.291	4.36	55.1		90
11:45	50	14.37	209	23	12.08	31.5	0.067	0.223	15.0	0.255	3.83	58.9		90.1
12:00	50	20.15	149	24	12.08	31.5	0.066	0.158	15.0	0.190	2.86	61.8		88.8
12:15	50	23.03	130	23.5	12.08	31.5	0.066	0.139	15.0	0.148	2.23	64.0		88.2
12:30	50	32.78	92	24	12.08	31.5	0.066	0.097	15.0	0.118	1.77	65.7		86.7
12:45	50	44.72	67	25	12.08	31.5	0.066	0.071	15.0	0.084	1.26	67.0		85.1
13:00	50	63.04	48	25.5	12.08	31.5	0.066	0.050	15.0	0.061	0.91	67.9		84.6
13:15	10	15.44	39	26	12.08	31.5	0.066	0.041	15.0	0.046	0.68	68.6		84.1
13:30	10	18.85	32	26	12.08	31.5	0.066	0.034	15.0	0.037	0.56	69.2		83.7
13:45	10	18.44	33	26.5	12.08	31.5	0.066	0.034	15.0	0.034	0.51	69.7		83.8
14:00	10	28.35	21	26	12.08	31.5	0.066	0.022	15.0	0.028	0.43	70.1		83.3
14:15	10	39.81	15	26	12.08	31.6	0.066	0.016	15.0	0.019	0.29	70.4		83
14:30	10	52.6	11	26.5	12.08	31.6	0.066	0.012	15.0	0.014	0.21	70.6		82.8
14:45	10	76.97	8	26.5	12.08	31.6	0.066	0.008	15.0	0.010	0.15	70.8		82.7
15:00	3	25.09	7	27	12.08	31.5	0.066	0.008	15.0	0.008	0.12	70.9		82.7
15:15	0	1	0	27	12.08	31.5	0.066	0.000	15.0	0.004	0.06	70.9		82.8
15:30	0	1	0	27	12.08	31.5	0.066	0.000	15.0	0.000	0.00	70.9		83.2
15:45	0	1	0	27	12.08	31.4	0.066	0.000	15.0	0.000	0.00	70.9		83
16:00	0	1	0	27.5	12.08	31.4	0.065	0.000	15.0	0.000	0.00	70.9		83
16:15	0	1	0	27.5	12.08	31.4	0.065	0.000	15.0	0.000	0.00	70.9		83
16:30	0	1	0	28	12.08	31.4	0.065	0.000	15.0	0.000	0.00	70.9		83.3
16:45	0	1	0	28	12.08	31.4	0.065	0.000	15.0	0.000	0.00	70.9		83.4
17:00	0	1	0	28.5	12.08	31.4	0.065	0.000	15.0	0.000	0.00	70.9		83.3
			185				Avg's:	0.145	480.0			69.6	Avg:	86.2

	S Kujawa											
	8/27/2003											
	TEST RUN	F-21										
Run Time	% O2	% CO2	% H2O	% CO	PPMv TCE	PPMv PCE	PPMv TCA	MW				
9:00	95.4%	0.4307%	4%	0.0001%	309	9.9	90.8	31.5				
9:05	95.3%	0.5168%	4%	0.0004%	309	9.9	90.8	31.5				
9:15	95.2%	0.6052%	4%	0.0011%	169.25			31.5				
9:30	95.1%	0.6936%	4%	0.0022%	29.5	10.6	1.55	31.5				
9:45	95.2%	0.5845%	4%	0.0030%	18.75			31.5				
10:00	95.3%	0.4754%	4%	0.0036%	8	9	1.55	31.5				
10:15	95.3%	0.4831%	4%	0.0042%	8			31.5				
10:30	95.3%	0.4908%	4%	0.0011%	8	7	1.55	31.5				
10:45	95.3%	0.4576%	4%	0.0015%	8			31.5				
11:00	95.4%	0.4244%	4%	0.0030%	8	7	1.55	31.5				
11:15	95.3%	0.5452%	4%	0.0044%	8			31.5				
11:30	95.1%	0.6659%	4%	0.0048%	8	7	1.55	31.5				
11:45	95.3%	0.5105%	4%	0.0048%	8			31.5				
12:00	95.4%	0.3551%	4%	0.0048%	8	7	1.55	31.5				
12:15	95.3%	0.5109%	4%	0.0040%	8			31.5				
12:30	95.1%	0.6667%	4%	0.0032%	8	7	1.55	31.5				
12:45	95.3%	0.5217%	4%	0.0032%	8			31.5				
13:00	95.4%	0.3766%	4%	0.0032%	8	7	1.55	31.5				
13:15	95.3%	0.5035%	4%	0.0032%	8			31.5				
13:30	95.2%	0.6303%	4%	0.0032%	8	7	1.55	31.5				
13:45	95.1%	0.7160%	4%	0.0047%	8			31.5				
14:00	95.0%	0.8016%	4%	0.0062%	8	7	1.55	31.5				
14:15	94.6%	1.1972%	4%	0.0062%	8			31.6				
14:30	94.2%	1.5927%	4%	0.0062%	8	7	1.55	31.6				
14:45	94.6%	1.1721%	4%	0.0171%	8			31.6				
15:00	95.0%	0.7515%	4%	0.0280%	8	7	1.55	31.5				
15:15	95.1%	0.7246%	4%	0.0280%	8			31.5				
15:30	95.3%	0.4687%	4%	0.0197%	8			31.5				
15:45	95.6%	0.2265%	4%	0.0113%	8			31.4				
16:00	95.6%	0.2146%	4%	0.0113%	8	7	1.55	31.4				
16:15	95.6%	0.2128%	4%	0.0113%	8			31.4				
16:30	95.6%	0.2109%	4%	0.0113%	8	7	1.55	31.4				
16:45	95.6%	0.2001%	4%	0.0113%	8.35			31.4				
17:00	95.6%	0.1893%	4%	0.0113%	8.7	7	1.55	31.4				

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S Kujawa 8/20/2003				Test Results	Str RPM:	Start		
TEST RUN	F-21							
	Results							
	Product slurry Sp. Gr.:	1.05						
	Final Product Slurry, ml:	370						
	Final Product Slurry, gm:	390.1						
	Dewar Flask net wt., gm	0.3031						
	Liquid/slurry Product, gm:	390.4		(Slurry Wt, 100% H2O2/O2 RXN):	404			
	Product Gas Weight, gm:	70.9						
	Product Wt, gm:	461.3						
	Total Charge Weight, gm:	474.2						
	Overall Mass Balance							
	Mass Balance Closure:	97.3%						
	Mass balance w/o gas:	82%						
	Species Mass Results			Species Mass Results				
	TriChloroEthylene		Anal. code	HexachloroBenzene		Anal. code		
	Slurry analysis, 1, mg/kg:	0.952 J		Slurry analysis, 1, mg/kg:	0.736 J			
	Slurry analysis, 2, mg/kg:	0.740 J		Slurry analysis, 2, mg/kg:	0.818 J			
	Avg., mg/kg	0.846		Avg., mg/kg	0.777			
	Total, mg:	0.330		Total, mg:	0.303			
	TCE, DRE, %	99.96%		HCb, DRE, %	95.61%			
	TetraChloroEthylene			Bi-Phenyl				
	Slurry analysis, 1, mg/kg:	1.960 U		Slurry analysis, 1, mg/kg:	4.940 U			
	Slurry analysis, 2, mg/kg:	1.950 U		Slurry analysis, 2, mg/kg:	4.450 U			
	Avg., mg/kg	1.955		Avg., mg/kg	4.695			
	Total, mg:	0.763		Total, mg:	1.832			
	PCE, DRE, %	98.96%		BP, DRE, %	47.67%	Run time:	8 Hours	
	1,1,1-TriChloroEthane			Aroclor 1260		Run Temp:	86.2 deg C	
	Slurry analysis, 1, mg/kg:	1.960 U		Slurry analysis, 1, mg/kg:	2.600	H2O2 vol:	250 ml	
	Slurry analysis, 2, mg/kg:	1.950 U		Slurry analysis, 2, mg/kg:				
	Avg., mg/kg	1.955		Avg., mg/kg	2.600			
	Total, mg:	0.763		Total, mg:	1.014			
	TCA, DRE, %	99.06%		Aroclor, DRE, %	79.71%			
	BEHP							
	Slurry analysis, 1, mg/kg:	22.800						
	Slurry analysis, 2, mg/kg:	25.700						
	Avg., mg/kg	24.250						
	Total, mg:	9.460						
	BEHP, DRE, %	94.17%						

[illegible]

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[illegible]

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S Kujawa									
7/30/2003									
TEST RUN	F-9A			Heat Balance					
	Condenser Bath			Oil Bath					
	Set Point Temperature, Deg C	5		Set Point Temperature, Deg C	100				
Time									
				Boss DS oil density, gm/ml	0.873				
				Boss DS oil heat cap. cal/gm/deg C	0.4				
11:32	Water Return Temp, Deg C	8.2		Oil Return Temp, Deg C	76.4				
	bucket ck volume, ml	100		bucket ck volume, ml	100				
	Bucket ck time, sec	17.97		Bucket ck time, sec	9.94				
	Flow rate, ml/min	334		Flow rate, ml/min	604				
	Enthalpy change, calorie/min:	1068		Enthalpy change, calorie/min:	-4975				
	Flask Top Surface Temp., C	73.6		Flask bottom Surface Temp., C	79.3				
	Flask Top Surface Temp., F	164		Flask bottom Surface Temp., F	175				
	Air Temp., F	79		Air Temp., F	79				
	Overall HT coef. Btu/hr/F/sq ft	2.75		Overall HT coef.	2.75				
	Top flask Area, in^2	188		bottom flask Area, in^2	265				
	emisivity	0.94		emisivity	0.94				
	Convective Loss, cal/min	1289		Convective Loss, cal/min	2035				
	Radiative Loss, cal/min	598		Radiative Loss, cal/min	970				
	Flask top Heat Loss, cal/min	1887		Flask bottom Heat Loss, cal/min	3005	4891			
	Reactor Temperature, C	87.8		P1 Gas Temp, Deg C.	27				
	Peroxide Temperature, F	79		Gas Flow Rate, gm/min	0.390			Correlated losses, cal/min	4442
	Peroxide Flow Rate, ml/min	2		Water Vap. gm/min	0.0115			Reflux Gas Delta H, cal/min	670
	Peroxide heat Cap, cal/gm/degC	0.8		P1 loss, H2O vapor, cal/min	6.39			Revised Acc/generation, cal/min	-255
	Peroxide Enthalpy Change, cal/min	118.4							
				Accumulation/Generation, cal/min	-1110				
12:51	Water Return Temp, Deg C	8.2		Oil Return Temp, Deg C	77.7				
	bucket ck volume, ml	100		bucket ck volume, ml	100				
	Bucket ck time, sec	17.72		Bucket ck time, sec	10.09				
	Flow rate, ml/min	339		Flow rate, ml/min	595				
	Enthalpy change, calorie/min:	1084		Enthalpy change, calorie/min:	-4631				
	Flask Top Surface Temp., C	74.6		Flask bottom Surface Temp., C	79.9				
	Flask Top Surface Temp., F	166		Flask bottom Surface Temp., F	176				
	Air Temp., F	83		Air Temp., F	83				
	Overall HT coef. Btu/hr/F/sq ft	3		Overall HT coef.	3				
	Top flask Area, in^2	188		bottom flask Area, in^2	265				
	emisivity	0.94		emisivity	0.94				
	Convective Loss, cal/min	1370		Convective Loss, cal/min	2152				
	Radiative Loss, cal/min	591		Radiative Loss, cal/min	952				
	Flask top Heat Loss, cal/min	1961		Flask bottom Heat Loss, cal/min	3104	5065			
	Reactor Temperature, C	89.5		P1 Gas Temp, Deg C.	29				
	Peroxide Temperature, F	83		Gas Flow Rate, gm/min	0.503			Correlated losses, cal/min	4309
	Peroxide Flow Rate, ml/min	2		Water Vap. gm/min	0.0148			Reflux Gas Delta H, cal/min	863
	Peroxide heat Cap, cal/gm/degC	0.8		P1 loss, H2O vapor, cal/min	8.24			Revised Acc/generation, cal/min	-659
	Peroxide Enthalpy Change, cal/min	117.4							
				Accumulation/Generation, cal/min	-1644				
15:05	Water Return Temp, Deg C	8.2		Oil Return Temp, Deg C	78				
	bucket ck volume, ml	100		bucket ck volume, ml	100				
	Bucket ck time, sec	17.44		Bucket ck time, sec	10.06				
	Flow rate, ml/min	344		Flow rate, ml/min	596				
	Enthalpy change, calorie/min:	1101		Enthalpy change, calorie/min:	-4582				
	Flask Top Surface Temp., C	75.6		Flask bottom Surface Temp., C	80.4				
	Flask Top Surface Temp., F	168		Flask bottom Surface Temp., F	177				
	Air Temp., F	86		Air Temp., F	86				
	Overall HT coef. Btu/hr/F/sq ft	3		Overall HT coef.	3				
	Top flask Area, in^2	188		bottom flask Area, in^2	265				
	emisivity	0.94		emisivity	0.94				
	Convective Loss, cal/min	1350		Convective Loss, cal/min	2104				
	Radiative Loss, cal/min	589		Radiative Loss, cal/min	939				
	Flask top Heat Loss, cal/min	1940		Flask bottom Heat Loss, cal/min	3043	4983			
	Reactor Temperature, C	87.7		P1 Gas Temp, Deg C.	31.5				
	Peroxide Temperature, F	86		Gas Flow Rate, gm/min	0.498			Correlated losses, cal/min	4143
	Peroxide Flow Rate, ml/min	0		Water Vap. gm/min	0.2296			Reflux Gas Delta H, cal/min	855
	Peroxide heat Cap, cal/gm/degC	0.8		P1 loss, H2O vapor, cal/min	127.41			Revised Acc/generation, cal/min	-415
	Peroxide Enthalpy Change, cal/min	0.0							
				Accumulation/Generation, cal/min	-1629				

S Kujawa	F-9A								
7/30/2003									
17:23	Water Return Temp, Deg C	8.9		Oil Return Temp, Deg C	77.7				
	bucket ck volume, ml	100		bucket ck volume, ml	100				
	Bucket ck time, sec	18.06		Bucket ck time, sec	9.75				
	Flow rate, ml/min	332		Flow rate, ml/min	615				
	Enthalpy change, calorie/min:	1296		Enthalpy change, calorie/min:	-4792				
	Flask Top Surface Temp., C	70.4		Flask bottom Surface Temp., C	79.4				
	Flask Top Surface Temp., F	159		Flask bottom Surface Temp., F	175				
	Air Temp., F	87		Air Temp., F	87				
	Overall HT coef. Btu/hr/F/sq ft	3		Overall HT coef.	3				
	Top flask Area, in^2	188		bottom flask Area, in^2	265				
	emisivity	0.94		emisivity	0.94				
	Convective Loss, cal/min	1180		Convective Loss, cal/min	2039				
	Radiative Loss, cal/min	503		Radiative Loss, cal/min	908				
	Flask top Heat Loss, cal/min	1683		Flask bottom Heat Loss, cal/min	2947	4630			
	Reactor Temperature, C	83.1		P1 Gas Temp. Deg C.	31				
	Peroxide Temperature, F	87		Gas Flow Rate, gm/min	0.530		Correlated losses, cal/min	4176	
	Peroxide Flow Rate, ml/min	0		Water Vap. gm/min	0.0000		Reflux Gas Delta H, cal/min	910	
	Peroxide heat Cap, cal/gm/degC	0.8		P1 loss, H2O vapor, cal/min	0.00		Revised Acc/generation, cal/min	-294	
	Peroxide Enthalpy Change, cal/min	0.0							
				Accumulation/Generation, cal/min	-1134				

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S Kujawa	F-10								
9/16/2003									
12:41	Water Return Temp, Deg C	8.1		Oil Return Temp, Deg C	77.3				
	bucket ck volume, ml	100		bucket ck volume, ml	100				
	Bucket ck time, sec	16.91		Bucket ck time, sec	10.06				
	Flow rate, ml/min	355		Flow rate, ml/min	596				
	Enthalpy change, calorie/min:	1100		Enthalpy change, calorie/min:	-4728				
	Flask Top Surface Temp., C	75.7		Flask bottom Surface Temp., C	76				
	Flask Top Surface Temp., F	168		Flask bottom Surface Temp., F	169				
	Air Temp., F	83		Air Temp., F	83				
	Overall HT coef. Btu/hr/F/sq ft	2.75		Overall HT coef.	2.75				
	Top flask Area, in^2	188		bottom flask Area, in^2	265				
	emisivty	0.94		emisivty	0.94				
	Convective Loss, cal/min	1286		Convective Loss, cal/min	1824				
	Radiative Loss, cal/min	608		Radiative Loss, cal/min	864				
	Flask top Heat Loss, cal/min	1894		Flask bottom Heat Loss, cal/min	2687	4581			
	Reactor Temperature, C	93.8		P1 Gas Temp. Deg C.	27.5				
	Peroxide Temperature, F	83		Gas Flow Rate, gm/min	0.398		Correlated losses, cal/min	4409	
	Peroxide Flow Rate, ml/min	0		Water Vap. gm/min	0.0176		Reflux Gas Delta H, cal/min	683	
	Peroxide heat Cap, cal/gm/degC	0.8		P1 loss, H2O vapor, cal/min	9.79		Revised Acc/generation, cal/min	-364	
	Peroxide Enthalpy Change, cal/r	0.0							
				Accumulation/Generation, cal/min	-963				
13:52	Water Return Temp, Deg C	8.9		Oil Return Temp, Deg C	79.1				
	bucket ck volume, ml	100		bucket ck volume, ml	100				
	Bucket ck time, sec	16.32		Bucket ck time, sec	10.12				
	Flow rate, ml/min	368		Flow rate, ml/min	593				
	Enthalpy change, calorie/min:	1434		Enthalpy change, calorie/min:	-4327				
	Flask Top Surface Temp., C	75.6		Flask bottom Surface Temp., C	77.3				
	Flask Top Surface Temp., F	168		Flask bottom Surface Temp., F	171				
	Air Temp., F	85		Air Temp., F	85				
	Overall HT coef. Btu/hr/F/sq ft	2.75		Overall HT coef.	2.75				
	Top flask Area, in^2	188		bottom flask Area, in^2	265				
	emisivty	0.94		emisivty	0.94				
	Convective Loss, cal/min	1253		Convective Loss, cal/min	1831				
	Radiative Loss, cal/min	595		Radiative Loss, cal/min	877				
	Flask top Heat Loss, cal/min	1848		Flask bottom Heat Loss, cal/min	2708	4556			
	Reactor Temperature, C	91.3		P1 Gas Temp. Deg C.	29.5				
	Peroxide Temperature, F	85		Gas Flow Rate, gm/min	0.173		Correlated losses, cal/min	4276	
	Peroxide Flow Rate, ml/min	0		Water Vap. gm/min	0.0051		Reflux Gas Delta H, cal/min	297	
	Peroxide heat Cap, cal/gm/degC	0.8		P1 loss, H2O vapor, cal/min	2.83		Revised Acc/generation, cal/min	-246	
	Peroxide Enthalpy Change, cal/r	0.0							
				Accumulation/Generation, cal/min	-1655				
15:33	Water Return Temp, Deg C	8.7		Oil Return Temp, Deg C	78.8				
	bucket ck volume, ml	100		bucket ck volume, ml	100				
	Bucket ck time, sec	16.46		Bucket ck time, sec	10.74				
	Flow rate, ml/min	365		Flow rate, ml/min	559				
	Enthalpy change, calorie/min:	1349		Enthalpy change, calorie/min:	-4136				
	Flask Top Surface Temp., C	71.5		Flask bottom Surface Temp., C	76				
	Flask Top Surface Temp., F	161		Flask bottom Surface Temp., F	169				
	Air Temp., F	89		Air Temp., F	89				
	Overall HT coef. Btu/hr/F/sq ft	2.75		Overall HT coef.	2.75				
	Top flask Area, in^2	188		bottom flask Area, in^2	265				
	emisivty	0.94		emisivty	0.94				
	Convective Loss, cal/min	1081		Convective Loss, cal/min	1696				
	Radiative Loss, cal/min	508		Radiative Loss, cal/min	815				
	Flask top Heat Loss, cal/min	1590		Flask bottom Heat Loss, cal/min	2511	4101			
	Reactor Temperature, C	86.7		P1 Gas Temp. Deg C.	30.5				
	Peroxide Temperature, F	89		Gas Flow Rate, gm/min	0.040		Correlated losses, cal/min	4209	
	Peroxide Flow Rate, ml/min	0		Water Vap. gm/min	0.0012		Reflux Gas Delta H, cal/min	69	
	Peroxide heat Cap, cal/gm/degC	0.8		P1 loss, H2O vapor, cal/min	0.66		Revised Acc/generation, cal/min	-142	
	Peroxide Enthalpy Change, cal/r	0.0							
				Accumulation/Generation, cal/min	-1314				
16:42	Water Return Temp, Deg C	8.2		Oil Return Temp, Deg C	76.3				
	bucket ck volume, ml	100		bucket ck volume, ml	100				
	Bucket ck time, sec	16.46		Bucket ck time, sec	10.74		Times from 15:33 data		
	Flow rate, ml/min	365		Flow rate, ml/min	559				
	Enthalpy change, calorie/min:	1166		Enthalpy change, calorie/min:	-4623				
	Flask Top Surface Temp., C	69.8		Flask bottom Surface Temp., C	74.8				
	Flask Top Surface Temp., F	158		Flask bottom Surface Temp., F	167				
	Air Temp., F	85		Air Temp., F	85				
	Overall HT coef. Btu/hr/F/sq ft	2.75		Overall HT coef.	2.75				
	Top flask Area, in^2	188		bottom flask Area, in^2	265				
	emisivty	0.94		emisivty	0.94				
	Convective Loss, cal/min	1095		Convective Loss, cal/min	1735				
	Radiative Loss, cal/min	506		Radiative Loss, cal/min	821				
	Flask top Heat Loss, cal/min	1601		Flask bottom Heat Loss, cal/min	2556	4158			
	Reactor Temperature, C	85.1		P1 Gas Temp. Deg C.	27				
	Peroxide Temperature, F	85		Gas Flow Rate, gm/min	0.013		Correlated losses, cal/min	4442	
	Peroxide Flow Rate, ml/min	0		Water Vap. gm/min	0.0004		Reflux Gas Delta H, cal/min	23	
	Peroxide heat Cap, cal/gm/degC	0.8		P1 loss, H2O vapor, cal/min	0.22		Revised Acc/generation, cal/min	-159	
	Peroxide Enthalpy Change, cal/r	0.0							
				Accumulation/Generation, cal/min	-701				

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S Kujawa	F-12	7/29/2003						
13:16	Water Return Temp, Deg C	8.2	Oil Return Temp, Deg C	79.7				
	bucket ck volume, ml	100	bucket ck volume, ml	100				
	Bucket ck time, sec	16.78	Bucket ck time, sec	9.56				
	Flow rate, ml/min	358	Flow rate, ml/min	628				
	Enthalpy change, calorie/min:	1144	Enthalpy change, calorie/min:	4449				
	Flask Top Surface Temp., C	79.9	Flask bottom Surface Temp., C	77				
	Flask Top Surface Temp., F	176	Flask bottom Surface Temp., F	171				
	Air Temp., F	82	Air Temp., F	82				
	Overall HT coef. Btu/hr/F/sq ft	3	Overall HT coef.	3				
	Top flask Area, in^2	188	bottom flask Area, in^2	265				
	emisivity	0.94	emisivity	0.94				
	Convective Loss, cal/min	1543	Convective Loss, cal/min	2054				
	Radiative Loss, cal/min	681	Radiative Loss, cal/min	894				
	Flask top Heat Loss, cal/min	2224	Flask bottom Heat Loss, cal/min	2948	5173			
	Reactor Temperature, C	89.2	P1 Gas Temp, Deg C	29				
	Peroxide Temperature, F	82	Gas Flow Rate, gm/min	0.437	Correlated losses, cal/min		4309	
	Peroxide Flow Rate, ml/min	2	Water Vap. gm/min	0.0129	Reflux Gas Delta H, cal/min		750	
	Peroxide heat Cap, cal/gm/degC	0.8	P1 loss, H2O vapor, cal/min	7.16	Revised Acc/generation, cal/min		-728	
	Peroxide Enthalpy Change, cal/min	117.9						
			Accumulation/Generation, cal/min	-1993				
14:17	Water Return Temp, Deg C	8.5	Oil Return Temp, Deg C	79.4				
	bucket ck volume, ml	100	bucket ck volume, ml	100				
	Bucket ck time, sec	18.6	Bucket ck time, sec	9.65				
	Flow rate, ml/min	323	Flow rate, ml/min	622				
	Enthalpy change, calorie/min:	1129	Enthalpy change, calorie/min:	4473				
	Flask Top Surface Temp., C	74.8	Flask bottom Surface Temp., C	75.8				
	Flask Top Surface Temp., F	167	Flask bottom Surface Temp., F	168				
	Air Temp., F	83	Air Temp., F	83				
	Overall HT coef. Btu/hr/F/sq ft	3	Overall HT coef.	3				
	Top flask Area, in^2	188	bottom flask Area, in^2	265				
	emisivity	0.94	emisivity	0.94				
	Convective Loss, cal/min	1376	Convective Loss, cal/min	1981				
	Radiative Loss, cal/min	594	Radiative Loss, cal/min	859				
	Flask top Heat Loss, cal/min	1970	Flask bottom Heat Loss, cal/min	2840	4810			
	Reactor Temperature, C	89.6	P1 Gas Temp, Deg C	29				
	Peroxide Temperature, F	83	Gas Flow Rate, gm/min	0.008	Correlated losses, cal/min		4309	
	Peroxide Flow Rate, ml/min	0	Water Vap. gm/min	0.0002	Reflux Gas Delta H, cal/min		14	
	Peroxide heat Cap, cal/gm/degC	0.8	P1 loss, H2O vapor, cal/min	0.14	Revised Acc/generation, cal/min		-149	
	Peroxide Enthalpy Change, cal/min	0.0						
			Accumulation/Generation, cal/min	-1467				
15:40	Water Return Temp, Deg C	9.2	Oil Return Temp, Deg C	79.3				
	bucket ck volume, ml	100	bucket ck volume, ml	100				
	Bucket ck time, sec	16.43	Bucket ck time, sec	9.65				
	Flow rate, ml/min	365	Flow rate, ml/min	622				
	Enthalpy change, calorie/min:	1534	Enthalpy change, calorie/min:	4494				
	Flask Top Surface Temp., C	76.6	Flask bottom Surface Temp., C	78.4				
	Flask Top Surface Temp., F	170	Flask bottom Surface Temp., F	173				
	Air Temp., F	83	Air Temp., F	83				
	Overall HT coef. Btu/hr/F/sq ft	3	Overall HT coef.	3				
	Top flask Area, in^2	188	bottom flask Area, in^2	265				
	emisivity	0.94	emisivity	0.94				
	Convective Loss, cal/min	1429	Convective Loss, cal/min	2090				
	Radiative Loss, cal/min	622	Radiative Loss, cal/min	918				
	Flask top Heat Loss, cal/min	2051	Flask bottom Heat Loss, cal/min	3007	5059			
	Reactor Temperature, C	87.5	P1 Gas Temp, Deg C	30				
	Peroxide Temperature, F	83	Gas Flow Rate, gm/min	0.181	Correlated losses, cal/min		4242	
	Peroxide Flow Rate, ml/min	0	Water Vap. gm/min	0.0053	Reflux Gas Delta H, cal/min		311	
	Peroxide heat Cap, cal/gm/degC	0.8	P1 loss, H2O vapor, cal/min	2.97	Revised Acc/generation, cal/min		-59	
	Peroxide Enthalpy Change, cal/min	0.0						
			Accumulation/Generation, cal/min	-2101				
19:10	Water Return Temp, Deg C	8.5	Oil Return Temp, Deg C	78.6				
	bucket ck volume, ml	100	bucket ck volume, ml	100				
	Bucket ck time, sec	18.47	Bucket ck time, sec	9.72				
	Flow rate, ml/min	325	Flow rate, ml/min	617				
	Enthalpy change, calorie/min:	1137	Enthalpy change, calorie/min:	4613				
	Flask Top Surface Temp., C	69.6	Flask bottom Surface Temp., C	75.5				
	Flask Top Surface Temp., F	157	Flask bottom Surface Temp., F	168				
	Air Temp., F	86	Air Temp., F	86				
	Overall HT coef. Btu/hr/F/sq ft	3	Overall HT coef.	3				
	Top flask Area, in^2	188	bottom flask Area, in^2	265				
	emisivity	0.94	emisivity	0.94				
	Convective Loss, cal/min	1173	Convective Loss, cal/min	1899				
	Radiative Loss, cal/min	497	Radiative Loss, cal/min	828				
	Flask top Heat Loss, cal/min	1670	Flask bottom Heat Loss, cal/min	2728	4397			
	Reactor Temperature, C	83.4	P1 Gas Temp, Deg C	30.5				
	Peroxide Temperature, F	86	Gas Flow Rate, gm/min	0.012	Correlated losses, cal/min		4209	
	Peroxide Flow Rate, ml/min	0	Water Vap. gm/min	0.0003	Reflux Gas Delta H, cal/min		20	
	Peroxide heat Cap, cal/gm/degC	0.8	P1 loss, H2O vapor, cal/min	0.19	Revised Acc/generation, cal/min		-384	
	Peroxide Enthalpy Change, cal/min	0.0						
			Accumulation/Generation, cal/min	-922				

Reactor Charge

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	S Kujawa											
	8/27/2003											
	TEST RUN		F-16									
Run Time	% O2	% CO2	% H2O	% CO	PPMv TCE	PPMv PCE	PPMv TCA	MW				
7:30	95.7%	0.1353%	4%	0.0039%	0	0	0	31.4				
7:35	95.7%	0.1353%	4%	0.0039%	16	0	0	31.4				
7:45	95.7%	0.1419%	4%	0.0039%	0	0	0	31.4				
8:00	95.7%	0.1485%	4%	0.0039%	0	9	0	31.4				
8:15	95.7%	0.1333%	4%	0.0039%	0	0	0	31.4				
8:30	95.7%	0.1180%	4%	0.0039%	0	0	0	31.4				
8:45	95.7%	0.0915%	4%	0.0039%	0	0	0	31.4				
9:00	95.7%	0.0650%	4%	0.0037%	0	0	0	31.4				
9:15	95.7%	0.0745%	4%	0.0035%	0	0	0	31.4				
9:30	95.7%	0.0839%	4%	0.0035%	0	0	0	31.4				
9:45	95.7%	0.0815%	4%	0.0035%	0	0	0	31.4				
10:00	95.7%	0.0791%	4%	0.0042%	0	0	0	31.4				
10:15	95.7%	0.1242%	4%	0.0049%	0	0	0	31.4				
10:30	95.6%	0.1693%	4%	0.0049%	0	0	0	31.4				
10:45	95.7%	0.1448%	4%	0.0049%	0	0	0	31.4				
11:00	95.7%	0.1202%	4%	0.0045%	0	0	0	31.4				
11:15	95.7%	0.0788%	4%	0.0041%	0	0	0	31.4				
11:30	95.8%	0.0374%	4%	0.0041%	0	0	0	31.4				
11:45	95.7%	0.0890%	4%	0.0041%	0	0	0	31.4				
12:00	95.7%	0.1405%	4%	0.0045%	0	0	0	31.4				
12:15	95.7%	0.1474%	4%	0.0048%	0	0	0	31.4				
12:30	95.6%	0.1542%	4%	0.0048%	0	0	0	31.4				
12:45	95.7%	0.1319%	4%	0.0048%	0	0	0	31.4				
13:00	95.7%	0.1085%	4%	0.0059%	0	0	0	31.4				
13:15	95.7%	0.1267%	4%	0.0070%	0	0	0	31.4				
13:30	95.7%	0.1438%	4%	0.0070%	0	0	0	31.4				
13:45	95.6%	0.1685%	4%	0.0070%	0	0	0	31.4				
14:00	95.6%	0.1932%	4%	0.0046%	0	0	0	31.4				
14:15	95.6%	0.1891%	4%	0.0022%	0	0	0	31.4				
14:30	95.6%	0.1849%	4%	0.0022%	0	0	0	31.4				
14:45	95.6%	0.2115%	4%	0.0022%	0	0	0	31.4				
15:00	95.6%	0.2381%	4%	0.0059%	0	0	0	31.4				
15:15	95.6%	0.1938%	4%	0.0095%	0	0	0	31.4				
15:30	95.6%	0.1494%	4%	0.0095%	0	0	0	31.4				
15:45	95.6%	0.1661%	4%	0.0095%	0	0	0	31.4				
16:00	95.6%	0.1827%	4%	0.0124%	0	0	0	31.4				
16:15	95.6%	0.1687%	4%	0.0153%	0	0	0	31.4				
16:30	95.6%	0.1546%	4%	0.0153%	0	0	0	31.4				
16:45	95.6%	0.2025%	4%	0.0153%	0	0	0	31.4				
17:00	95.5%	0.2503%	4%	0.0153%	0	0	0	31.4				
17:15	95.6%	0.2022%	4%	0.0153%	0	0	0	31.4				
17:30	95.6%	0.1541%	4%	0.0153%	0	0	0	31.4				
17:45	95.6%	0.1694%	4%	0.0153%	0	0	0	31.4				
18:00	95.6%	0.1846%	4%	0.0153%	0	0	0	31.4				
18:15	95.6%	0.1771%	4%	0.0153%	0	0	0	31.4				
18:30	95.6%	0.1696%	4%	0.0153%	0	0	0	31.4				
18:45	95.6%	0.1621%	4%	0.0153%	0	0	0	31.4				
19:00	95.6%	0.1545%	4%	0.0153%	0	0	0	31.4				
19:15	95.6%	0.1552%	4%	0.0153%	0	0	0	31.4				
19:30	95.6%	0.1558%	4%	0.0153%	0	0	0	31.4				

MSE-TA

TEST RESULTS

	S Kujawa													
	8/27/2003													
	TEST RUN	F-16												
	Instantaneous rates:							Integrated quantities:						
	O ₂ gm/min	CO ₂ g/m	H ₂ O g/m	CO g/m	TCE g/m	PCE g/m	TCA g/m	O ₂ gm	CO ₂ gm	H ₂ O gm	CO gm	TCE gm	PCE gm	TCA gm
Run Time														
7:30	0.3309	0.0006	0.0082	1.18E-05	0.0000	0.0000	0.0000	0.000	0.000643427	0.008162375	1.18024E-05	0.00E+00	0.00E+00	0.00E+00
7:35	0.3058	0.0006	0.0075	1.09E-05	0.0000	0.0000	0.0000	1.592	0.004	0.047	0.000	5.23E-05	0.00E+00	0.00E+00
7:45	0.4433	0.0009	0.0109	1.58E-05	0.0000	0.0000	0.0000	5.337	0.011	0.140	0.000	1.57E-04	0.00E+00	0.00E+00
8:00	0.4517	0.0010	0.0111	1.61E-05	0.0000	0.0000	0.0000	12.049	0.025	0.305	0.000	1.57E-04	1.65E-04	0.00E+00
8:15	0.4422	0.0008	0.0109	1.58E-05	0.0000	0.0000	0.0000	18.753	0.039	0.471	0.001	1.57E-04	3.31E-04	0.00E+00
8:30	0.4292	0.0007	0.0106	1.53E-05	0.0000	0.0000	0.0000	25.289	0.051	0.632	0.001	1.57E-04	3.31E-04	0.00E+00
8:45	0.3600	0.0005	0.0089	1.28E-05	0.0000	0.0000	0.0000	31.208	0.060	0.778	0.001	1.57E-04	3.31E-04	0.00E+00
9:00	0.4080	0.0004	0.0101	1.38E-05	0.0000	0.0000	0.0000	36.968	0.066	0.920	0.001	1.57E-04	3.31E-04	0.00E+00
9:15	0.4019	0.0004	0.0099	1.29E-05	0.0000	0.0000	0.0000	43.042	0.072	1.070	0.002	1.57E-04	3.31E-04	0.00E+00
9:30	0.4174	0.0005	0.0103	1.34E-05	0.0000	0.0000	0.0000	49.187	0.079	1.221	0.002	1.57E-04	3.31E-04	0.00E+00
9:45	0.4049	0.0005	0.0100	1.30E-05	0.0000	0.0000	0.0000	55.354	0.086	1.373	0.002	1.57E-04	3.31E-04	0.00E+00
10:00	0.3991	0.0005	0.0098	1.53E-05	0.0000	0.0000	0.0000	61.385	0.093	1.522	0.002	1.57E-04	3.31E-04	0.00E+00
10:15	0.4088	0.0007	0.0101	1.83E-05	0.0000	0.0000	0.0000	67.444	0.102	1.671	0.002	1.57E-04	3.31E-04	0.00E+00
10:30	0.4153	0.0010	0.0102	1.86E-05	0.0000	0.0000	0.0000	73.625	0.115	1.824	0.003	1.57E-04	3.31E-04	0.00E+00
10:45	0.4176	0.0009	0.0103	1.87E-05	0.0000	0.0000	0.0000	79.872	0.129	1.978	0.003	1.57E-04	3.31E-04	0.00E+00
11:00	0.4289	0.0007	0.0106	1.77E-05	0.0000	0.0000	0.0000	86.221	0.142	2.135	0.003	1.57E-04	3.31E-04	0.00E+00
11:15	0.4116	0.0005	0.0101	1.54E-05	0.0000	0.0000	0.0000	92.524	0.151	2.290	0.003	1.57E-04	3.31E-04	0.00E+00
11:30	0.4227	0.0002	0.0104	1.58E-05	0.0000	0.0000	0.0000	98.781	0.156	2.444	0.004	1.57E-04	3.31E-04	0.00E+00
11:45	0.3906	0.0005	0.0096	1.46E-05	0.0000	0.0000	0.0000	104.881	0.161	2.595	0.004	1.57E-04	3.31E-04	0.00E+00
12:00	0.3383	0.0007	0.0083	1.38E-05	0.0000	0.0000	0.0000	110.348	0.170	2.730	0.004	1.57E-04	3.31E-04	0.00E+00
12:15	0.2868	0.0006	0.0071	1.26E-05	0.0000	0.0000	0.0000	115.037	0.180	2.845	0.004	1.57E-04	3.31E-04	0.00E+00
12:30	0.2341	0.0005	0.0058	1.03E-05	0.0000	0.0000	0.0000	118.944	0.188	2.942	0.005	1.57E-04	3.31E-04	0.00E+00
12:45	0.2019	0.0004	0.0050	8.86E-06	0.0000	0.0000	0.0000	122.214	0.195	3.022	0.005	1.57E-04	3.31E-04	0.00E+00
13:00	0.1666	0.0003	0.0041	8.99E-06	0.0000	0.0000	0.0000	124.977	0.200	3.091	0.005	1.57E-04	3.31E-04	0.00E+00
13:15	0.1354	0.0002	0.0033	8.67E-06	0.0000	0.0000	0.0000	127.241	0.204	3.146	0.005	1.57E-04	3.31E-04	0.00E+00
13:30	0.1173	0.0002	0.0029	7.51E-06	0.0000	0.0000	0.0000	129.136	0.207	3.193	0.005	1.57E-04	3.31E-04	0.00E+00
13:45	0.0982	0.0002	0.0024	6.29E-06	0.0000	0.0000	0.0000	130.752	0.211	3.233	0.005	1.57E-04	3.31E-04	0.00E+00
14:00	0.0855	0.0002	0.0021	3.60E-06	0.0000	0.0000	0.0000	132.130	0.214	3.267	0.005	1.57E-04	3.31E-04	0.00E+00
14:15	0.0285	0.0001	0.0007	5.74E-07	0.0000	0.0000	0.0000	132.985	0.217	3.288	0.005	1.57E-04	3.31E-04	0.00E+00
14:30	0.0592	0.0002	0.0015	1.19E-06	0.0000	0.0000	0.0000	133.643	0.219	3.304	0.005	1.57E-04	3.31E-04	0.00E+00
14:45	0.0361	0.0001	0.0009	7.27E-07	0.0000	0.0000	0.0000	134.358	0.221	3.322	0.005	1.57E-04	3.31E-04	0.00E+00
15:00	0.0451	0.0002	0.0011	2.42E-06	0.0000	0.0000	0.0000	134.967	0.223	3.337	0.005	1.57E-04	3.31E-04	0.00E+00
15:15	0.0333	0.0001	0.0008	2.90E-06	0.0000	0.0000	0.0000	135.555	0.224	3.352	0.005	1.57E-04	3.31E-04	0.00E+00
15:30	0.0362	0.0001	0.0009	3.15E-06	0.0000	0.0000	0.0000	136.077	0.226	3.364	0.005	1.57E-04	3.31E-04	0.00E+00
15:45	0.0296	0.0001	0.0007	2.57E-06	0.0000	0.0000	0.0000	136.571	0.227	3.377	0.005	1.57E-04	3.31E-04	0.00E+00
16:00	0.0198	0.0001	0.0005	2.25E-06	0.0000	0.0000	0.0000	136.942	0.228	3.386	0.005	1.57E-04	3.31E-04	0.00E+00
16:15	0.0243	0.0001	0.0006	3.40E-06	0.0000	0.0000	0.0000	137.272	0.229	3.394	0.006	1.57E-04	3.31E-04	0.00E+00
16:30	0.0164	0.0000	0.0004	2.29E-06	0.0000	0.0000	0.0000	137.577	0.229	3.401	0.006	1.57E-04	3.31E-04	0.00E+00
16:45	0.0164	0.0000	0.0004	2.30E-06	0.0000	0.0000	0.0000	137.823	0.230	3.408	0.006	1.57E-04	3.31E-04	0.00E+00
17:00	0.0132	0.0000	0.0003	1.85E-06	0.0000	0.0000	0.0000	138.045	0.231	3.413	0.006	1.57E-04	3.31E-04	0.00E+00
17:15	0.0117	0.0000	0.0003	1.63E-06	0.0000	0.0000	0.0000	138.231	0.231	3.418	0.006	1.57E-04	3.31E-04	0.00E+00
17:30	0.0098	0.0000	0.0002	1.37E-06	0.0000	0.0000	0.0000	138.392	0.232	3.422	0.006	1.57E-04	3.31E-04	0.00E+00
17:45	0.0112	0.0000	0.0003	1.56E-06	0.0000	0.0000	0.0000	138.549	0.232	3.425	0.006	1.57E-04	3.31E-04	0.00E+00
18:00	0.0101	0.0000	0.0003	1.42E-06	0.0000	0.0000	0.0000	138.709	0.232	3.429	0.006	1.57E-04	3.31E-04	0.00E+00
18:15	0.0079	0.0000	0.0002	1.10E-06	0.0000	0.0000	0.0000	138.845	0.233	3.433	0.006	1.57E-04	3.31E-04	0.00E+00
18:30	0.0086	0.0000	0.0002	1.21E-06	0.0000	0.0000	0.0000	138.968	0.233	3.436	0.006	1.57E-04	3.31E-04	0.00E+00
18:45	0.0069	0.0000	0.0002	9.62E-07	0.0000	0.0000	0.0000	139.085	0.233	3.439	0.006	1.57E-04	3.31E-04	0.00E+00
19:00	0.0000	0.0000	0.0000	0.00E+00	0.0000	0.0000	0.0000	139.136	0.233	3.440	0.006	1.57E-04	3.31E-04	0.00E+00
19:15	0.0000	0.0000	0.0000	0.00E+00	0.0000	0.0000	0.0000	139.136	0.233	3.440	0.006	1.57E-04	3.31E-04	0.00E+00
19:30	0.0000	0.0000	0.0000	0.00E+00	0.0000	0.0000	0.0000	139.136	0.233	3.440	0.006	1.57E-04	3.31E-04	0.0000E+00
								O ₂ gm	CO ₂ gm	H ₂ O gm	CO gm	TCE gm	PCE gm	TCA gm
								Sum of components=		142.82				
								VOC in gas/VOC fed				0.018%	0.441%	0.000%

S Kujawa 8/18/2003									
				Test Results	Str RPM:		Start		
TEST RUN	F-16								
	Results								
	Product slurry Sp. Gr.:	1.04							
	Final Product Slurry, ml:	595							
	Final Product Slurry, gm:	619.4							
	Dewar Flask net wt., gm	0.6152							
	Liquid/slurry Product, gm:	620.0		(Slurry Wt, 100% H2O2/O2 RXN):	635				
	Product Gas Weight, gm:	142.3							
	Product Wt, gm:	762.3							
	Total Charge Weight, gm:	776.3							
	Overall Mass Balance								
	Mass Balance Closure:	98.2%							
	Mass balance w/o gas:	80%							
	Species Mass Results			Species Mass Results					
	TriChloroEthylene		Anal. code	HexachloroBenzene		Anal. code			
	Slurry analysis, 1, mg/kg:	1.930 U		Slurry analysis, 1, mg/kg:	0.605 J				
	Slurry analysis, 2, mg/kg:	1.960 U		Slurry analysis, 2, mg/kg:	4.920 J				
	Avg., mg/kg	1.945		Avg., mg/kg	2.763				
	Total, mg:	1.205		Total, mg:	1.711				
	TCE, DRE, %	99.86%		HCb, DRE, %	71.48%				
	TetraChloroEthylene			Bi-Phenyl					
	Slurry analysis, 1, mg/kg:	1.930 U		Slurry analysis, 1, mg/kg:	4.730 U				
	Slurry analysis, 2, mg/kg:	1.960 U		Slurry analysis, 2, mg/kg:	4.920 U				
	Avg., mg/kg	1.945		Avg., mg/kg	4.825				
	Total, mg:	1.205		Total, mg:	2.989				
	PCE, DRE, %	98.39%		BP, DRE, %	0.38%		Run time:	12 Hours	
							Run Temp:	89.1 deg C	
							H2O2 vol:	500 ml	
	1,1,1-TriChloroEthane			Aroclor 1260					
	Slurry analysis, 1, mg/kg:	1.930 U		Slurry analysis, 1, mg/kg:	1.600				
	Slurry analysis, 2, mg/kg:	1.960 U		Slurry analysis, 2, mg/kg:					
	Avg., mg/kg	1.945		Avg., mg/kg	1.600				
	Total, mg:	1.205		Total, mg:	0.991				
	TCA, DRE, %	98.51%		Aroclor, DRE, %	92.66%				
	BEHP								
	Slurry analysis, 1, mg/kg:	29.500							
	Slurry analysis, 2, mg/kg:	27.400							
	Avg., mg/kg	28.450							
	Total, mg:	17.622							
	BEHP, DRE, %	89.36%							
	VOA and SVOA								
	not yet available. DRE is a place holder.								
	Stk 8/11/03								

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C-62

TEST RESULTS

[illegible]

S Kujawa															
9/3/2003															
TEST RUN															
F-22															
Run Time	Gas Vol, cc	Time, sec	accm	Temp, C	P baro psia	MW	Density lb/ft ³	gm/min	Time delta min.	Rate avg gm/min	Mass delta gm	Mass sum gm	Rctr T Deg C		
8:30		1	0	22	12.13	31.7	0.067	0.000	0.0	0.000	0.00	0.0			82.2
8:35	50	16.75	179	21	12.13	32.2	0.069	0.197	5.0	0.099	0.49	0.5			83.2
8:45	50	9	333	21	12.13	31.8	0.068	0.363	10.0	0.280	2.80	3.3			85.5
9:00	50	7.88	381	21	12.13	31.8	0.068	0.414	15.0	0.389	5.83	9.1			91.5
9:15	50	7.75	387	21	12.13	31.8	0.068	0.421	15.0	0.418	6.26	15.4			91.4
9:30	50	7.19	417	21	12.13	31.8	0.068	0.454	15.0	0.438	6.56	22.0			92.7
9:45	50	7.22	416	21	12.13	31.8	0.068	0.452	15.0	0.453	6.79	28.8			92.8
10:00	50	7.13	421	21	12.13	31.8	0.068	0.458	15.0	0.455	6.82	35.6			92.9
10:15	50	7.115	422	21	12.13	31.8	0.068	0.459	15.0	0.458	6.88	42.5			93
10:30	50	7.69	390	23	12.13	31.8	0.067	0.422	15.0	0.440	6.60	49.1			92.9
10:45	50	7.72	389	21	12.13	31.8	0.068	0.423	15.0	0.422	6.34	55.4			92.7
11:00	50	8.25	364	22	12.13	31.8	0.068	0.394	15.0	0.409	6.13	61.5			91.8
11:15	50	8.22	365	22	12.13	31.8	0.068	0.396	15.0	0.395	5.93	67.5			91.7
11:30	50	7.69	390	23	12.13	31.8	0.067	0.422	15.0	0.408	6.12	73.6			91.9
11:45	50	7.72	389	24	12.13	31.8	0.067	0.419	15.0	0.420	6.30	79.9			92.3
12:00	50	7.59	395	24	12.13	31.8	0.067	0.426	15.0	0.422	6.33	86.2			92.5
12:15	50	7.5	400	25	12.13	31.8	0.067	0.429	15.0	0.428	6.41	92.6			92.8
12:30	50	7.62	394	24	12.13	31.8	0.067	0.424	15.0	0.427	6.40	99.0			92.5
12:45	50	7.56	397	25.5	12.13	31.8	0.067	0.425	15.0	0.425	6.37	105.4			92.4
13:00	50	7.72	389	26.5	12.13	31.8	0.067	0.415	15.0	0.420	6.30	111.7			92.5
13:15	50	7.6	395	26.5	12.13	31.8	0.067	0.422	15.0	0.418	6.28	118.0			92.3
13:30	50	7.68	391	27	12.13	31.8	0.067	0.417	15.0	0.419	6.29	124.3			93
13:45	50	8.53	352	27	12.13	31.8	0.067	0.375	15.0	0.396	5.94	130.2			93
14:00	50	9.47	317	29	12.13	31.8	0.066	0.336	15.0	0.355	5.33	135.5			92.6
14:15	50	10.82	277	29	12.13	31.8	0.066	0.294	15.0	0.315	4.72	140.3			92.2
14:30	50	12.25	245	29	12.13	31.8	0.066	0.260	15.0	0.277	4.15	144.4			91.8
14:45	50	13.4	224	29	12.13	31.8	0.066	0.237	15.0	0.248	3.73	148.1			91.3
15:00	50	14.37	209	25	12.13	31.8	0.067	0.224	15.0	0.231	3.46	151.6			90.7
15:15	50	17.44	172	29	12.13	31.8	0.066	0.182	15.0	0.203	3.05	154.7			90.3
15:30	50	19.38	155	29	12.13	31.8	0.066	0.164	15.0	0.173	2.60	157.3			90
15:45	50	22.34	134	29	12.13	31.8	0.066	0.143	15.0	0.153	2.30	159.6			89.9
16:00	50	25.5	118	29	12.13	31.8	0.066	0.125	15.0	0.134	2.01	161.6			89.3
16:15	50	28.72	104	29	12.13	31.8	0.066	0.111	15.0	0.118	1.77	163.3			89.3
16:30	10	6.6	91	29	12.13	31.8	0.066	0.097	15.0	0.104	1.56	164.9			89.3
16:45	10	7.25	83	29	12.13	31.8	0.066	0.088	15.0	0.092	1.38	166.3			88.6
17:00	10	8.47	71	29	12.13	31.8	0.066	0.075	15.0	0.082	1.22	167.5			88.9
17:15	10	8.94	67	29	12.13	31.9	0.066	0.071	15.0	0.073	1.10	168.6			88.6
17:30	10	11.25	53	29	12.13	31.9	0.066	0.057	15.0	0.064	0.96	169.5			88.3
17:45	10	11.93	50	28	12.13	31.9	0.066	0.054	15.0	0.055	0.83	170.4			88.9
18:00	10	13.37	45	28	12.13	31.9	0.067	0.048	15.0	0.051	0.76	171.1			88.8
18:15	10	13.37	45	28	12.13	31.9	0.067	0.048	15.0	0.048	0.72	171.9			88.7
18:30	10	16.47	36	28	12.13	31.9	0.067	0.039	15.0	0.043	0.65	172.5			88.2
18:45	10	18.69	32	28	12.13	31.9	0.067	0.034	15.0	0.037	0.55	173.0			88
19:00	10	21.44	28	28	12.13	31.9	0.067	0.030	15.0	0.032	0.48	173.5			87
19:15	10	24.43	25	27	12.13	31.9	0.067	0.026	15.0	0.028	0.42	174.0			86.5
19:30	10	30.69	20	25	12.13	31.9	0.067	0.021	15.0	0.024	0.36	174.3			86.1
19:45	10	35.59	24	25	12.13	31.9	0.067	0.025	15.0	0.023	0.35	174.7			85.3
20:00	10	32.81	18	23	12.13	31.9	0.068	0.020	15.0	0.023	0.34	175.0			86
20:15	10	34.19	18	25	12.13	31.9	0.067	0.019	15.0	0.019	0.29	175.3			87.1
20:30	10	33.72	18	25	12.13	31.9	0.067	0.019	15.0	0.019	0.29	175.6			87.8
Avg's:								0.237	720.0			171.0	Avg:		

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